

Non-linear model predictive control of a small-scale fourth generation district heating network with on/off heat pumps

ISEC 2022

Jelger Jansen, Lieve Helsen

07/04/2022

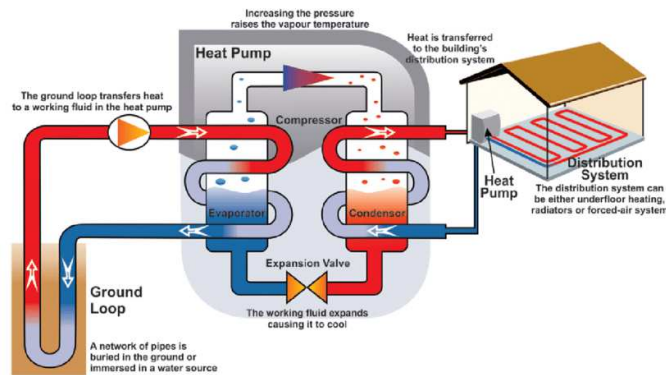
Introduction

European Green Deal → climate neutral in 2050



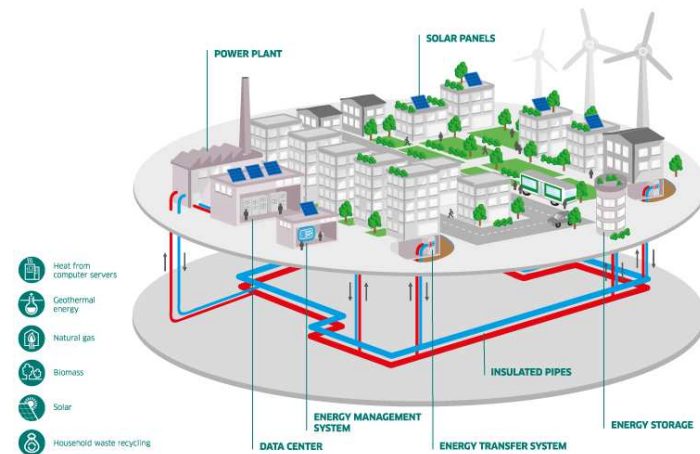
Decarbonisation of the residential heating sector

Rural areas



https://www.researchgate.net/figure/Geothermal-heat-pump-schematic-in-heating-mode_fig2_316919670

Urban areas



<https://www.engie.com/en/businesses/district-heating-cooling-systems>

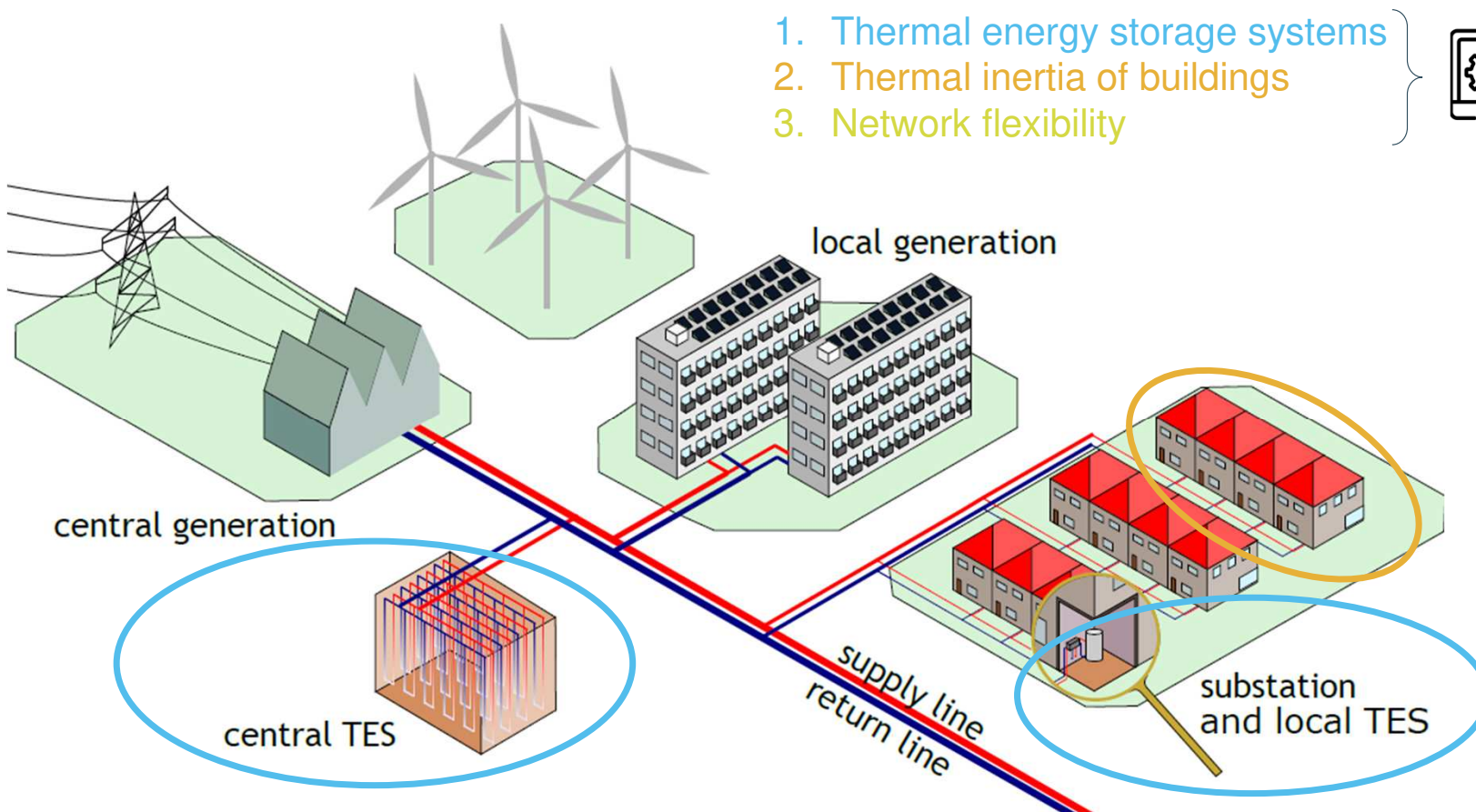
Fourth generation district heating

1. Thermal energy storage systems
2. Thermal inertia of buildings
3. Network flexibility

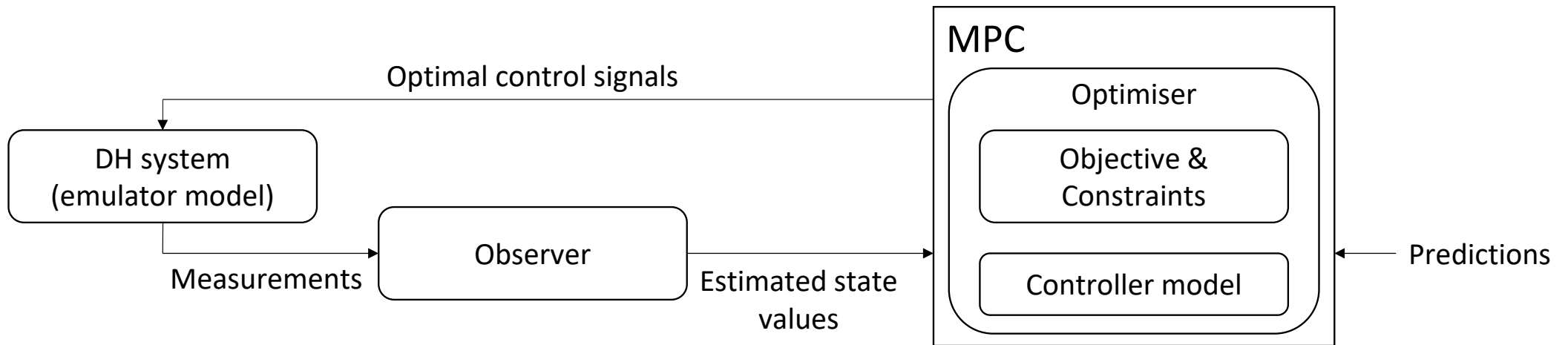


supply=demand

$\min J$



Model predictive control



MPC of 4GDH systems

4GDH systems

- Flexibility
- Non-linearities (pressure-mass flow relation, COP HP, ...)
- Integers (on/off HP, on/off circulation pump, ...)

Literature

- MPC optimal control problems: either LP, MILP, or NLP
- Limited complexity and flexibility

My presentation

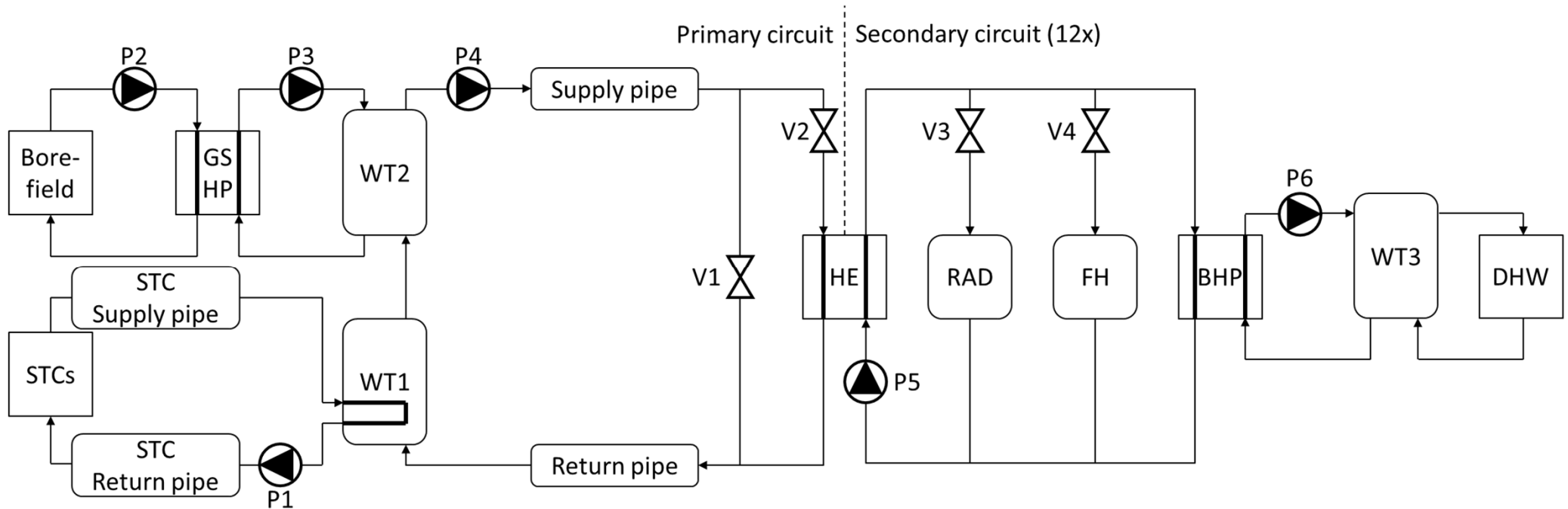
- NLP-based MPC to control a small-scale 4GDH network with on/off heat pumps
- MPC can exploit flexibility of both TES systems and thermal building inertia

Almshouses *De Schipjes*

- Social housing neighbourhood (12 buildings)
- Retrofitted buildings
- 4GDH network



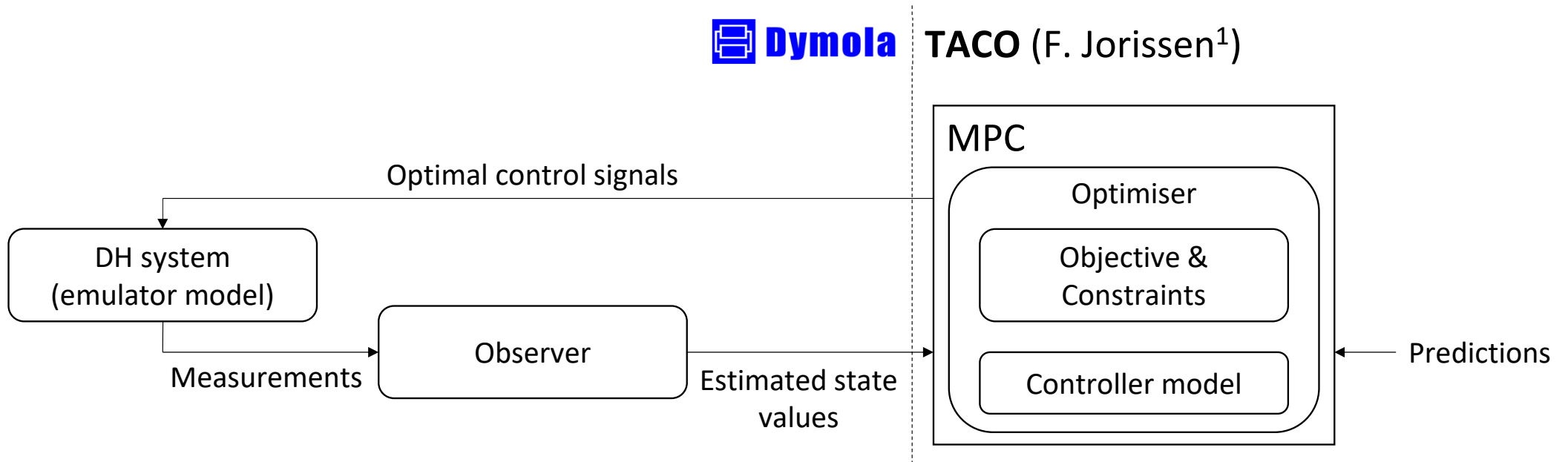
De Schipjes – DH network



Model-in-the-loop approach

MPC settings

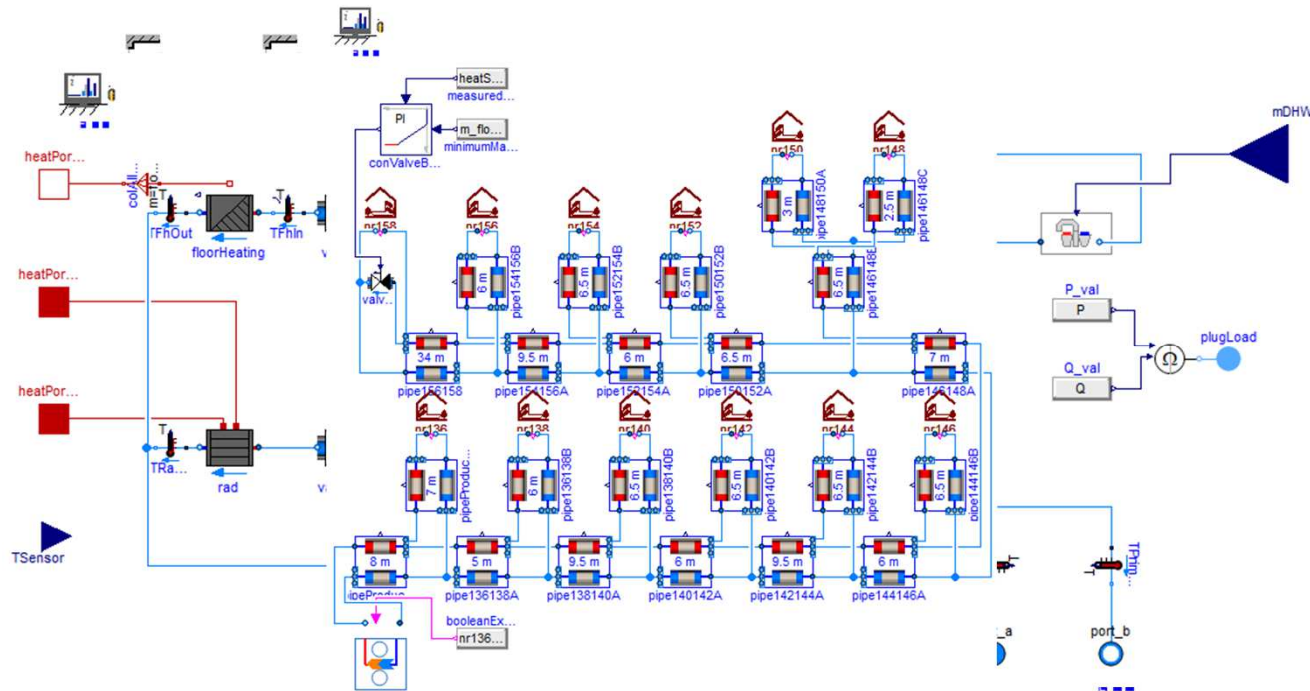
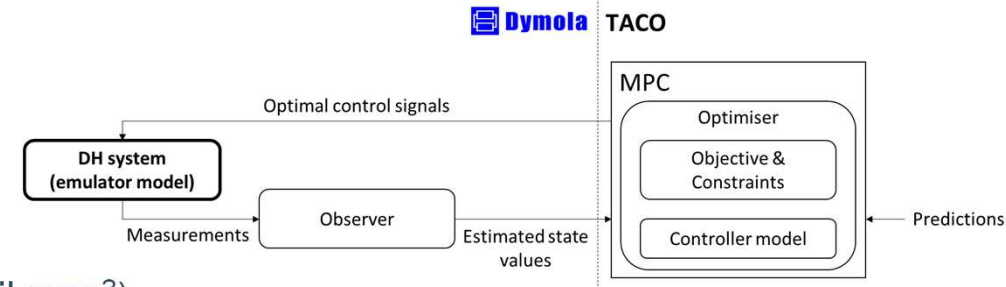
- $\Delta t_{prediction} = 2$ days
- $\Delta t_{control} = 15$ minutes
- Perfect predictions



[1] F. Jorissen, W. Boydens, and L. Helsen, "TACO, an automated toolchain for model predictive control of building systems: implementation and verification," *J. Build. Perform. Simul.*, vol. 12, no. 2, pp. 180–192, 2019.

Emulator model

- White-box modelling approach
- Modelica modelling language (IDEAS² and Buildings library³)



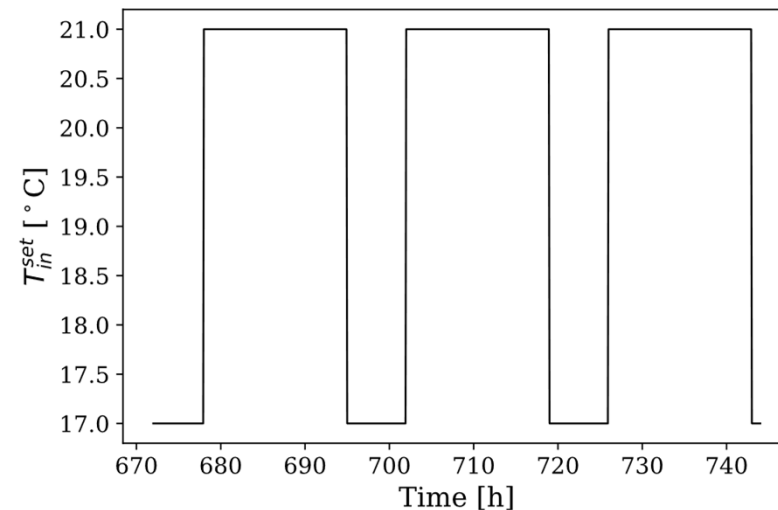
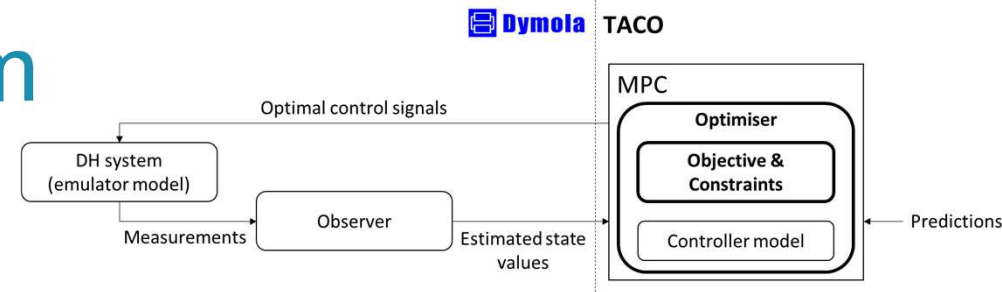
[2] F. Jorissen, G. Reynders, R. Baetens, D. Picard, D. Saelens, and L. Helsens, "Implementation and verification of the IDEAS building energy simulation library," *J. Build. Perform. Simul.*, vol. 11, no. 6, pp. 669–688, 2018.

[3] M. Wetter, W. Zuo, T. S. Noudui, and X. Pang, "Modelica Buildings library," *J. Build. Perform. Simul.*, vol. 7, no. 4, pp. 253–270, 2014.

MPC's optimisation problem

Objective and constraints

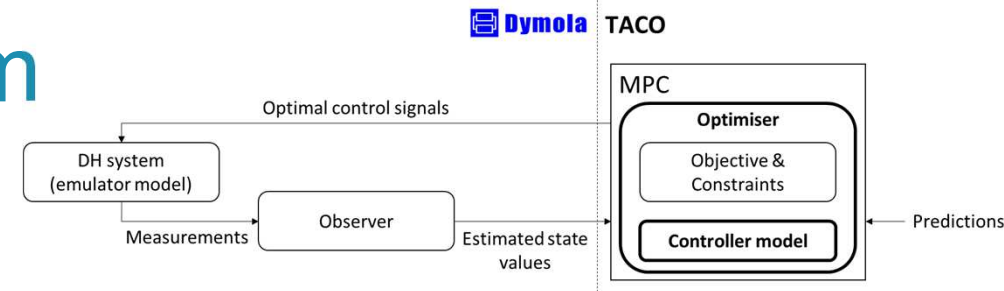
$$\begin{aligned} \min J(t) = & P_{GSHP}(t) + P_{P1}(t) + P_{P4}(t) \\ & + \sum_{i=1}^{12} (P_{BHP,i}(t) + P_{P5,i}(t)) \\ & + \sum_{i=1}^{12} (w_{SH} s_{i,SH}(t)^2 + w_{DHW} s_{i,DHW}(t)^2) \\ \text{s.t. } & T_{in}^{set}(t) - s_{i,SH}(t) \leq T_{in}(t) \\ & T_{DHW}^{set}(t) - s_{i,DHW}(t) \leq T_{DHW}(t) = 45^{\circ}\text{C} \\ & s_{i,SH}(t), s_{i,DHW}(t) \geq 0 \end{aligned}$$



MPC's optimisation problem

Objective and constraints

$$\begin{aligned} \min J(t) = & P_{GSHP}(t) + P_{P1}(t) + P_{P4}(t) \\ & + \sum_{i=1}^{12} (P_{BHP,i}(t) + P_{P5,i}(t)) \\ & + \sum_{i=1}^{12} (w_{SH} s_{i,SH}(t)^2 + w_{DHW} s_{i,DHW}(t)^2) \\ \text{s.t. } & T_{in}^{set}(t) - s_{i,SH}(t) \leq T_{in}(t) \\ & T_{DHW}^{set}(t) - s_{i,DHW}(t) \leq T_{DHW}(t) \\ & s_{i,SH}(t), s_{i,DHW}(t) \geq 0 \end{aligned}$$

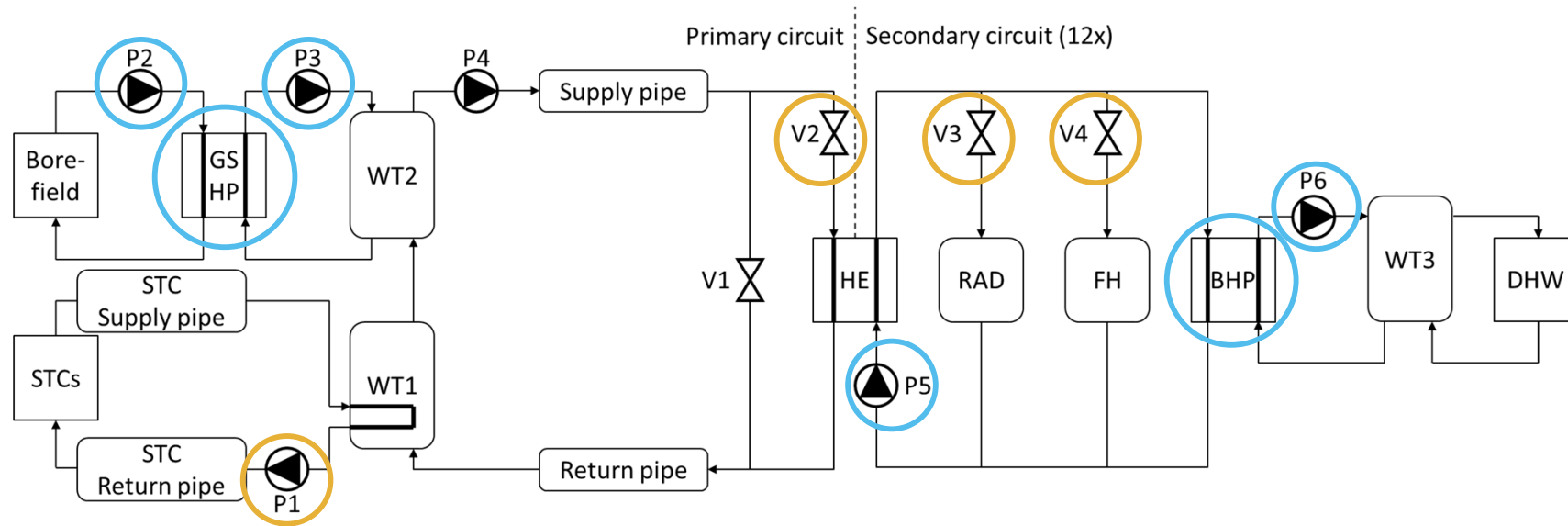
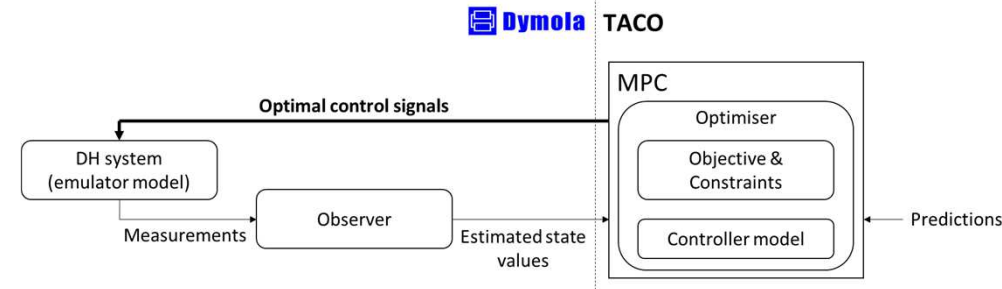


Controller model

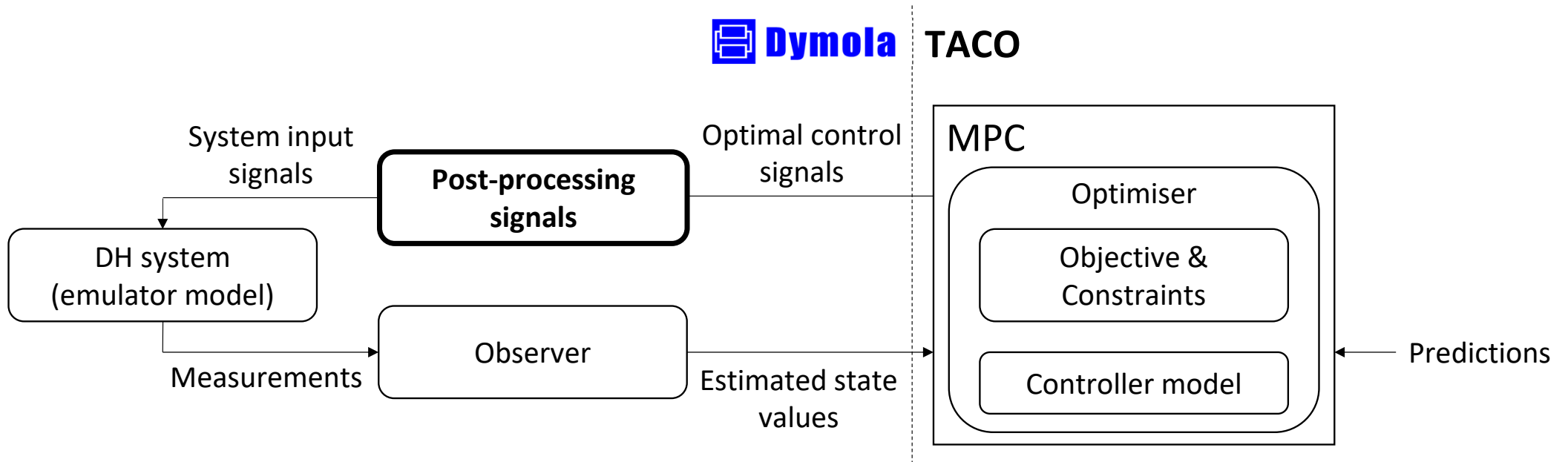
- Derived from emulator model
- In-house developed component models (optimisation-oriented)

Optimal control signals

- Real-life system → **continuous** and **integer** inputs
- TACO → continuous optimisation variables



Model-in-the-loop approach



Post-processing signals

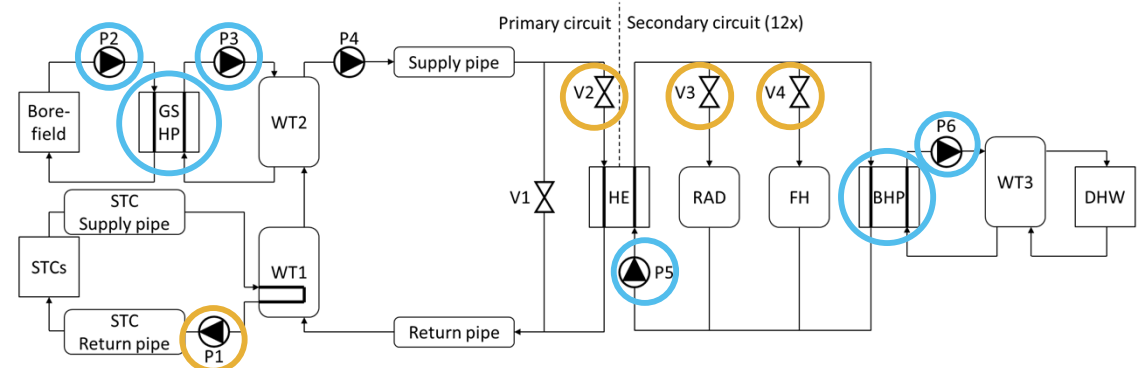
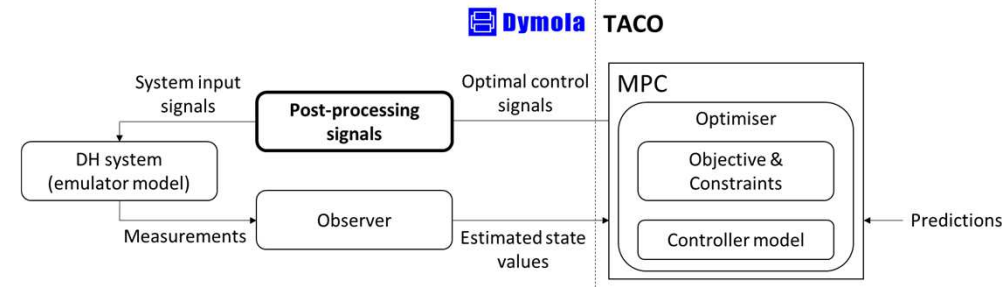
- Circulation pumps
 - P2, P3 ~ GSHP
 - P6 ~ BHP
 - P5 ~ Heat demand building
- HPs

1. Tank method

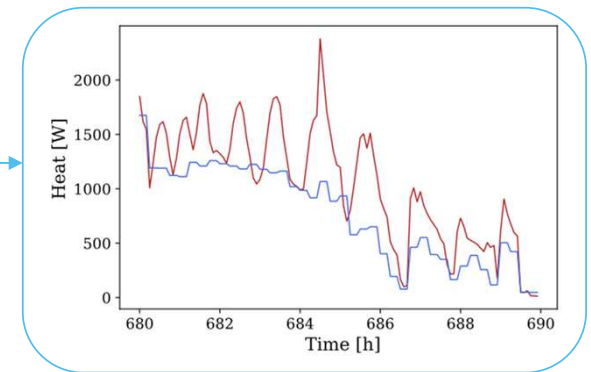
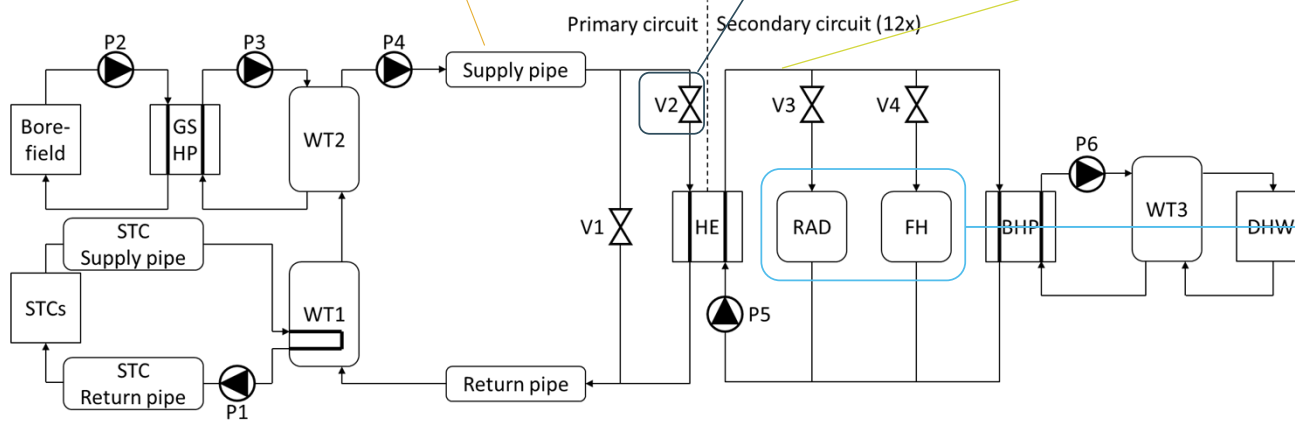
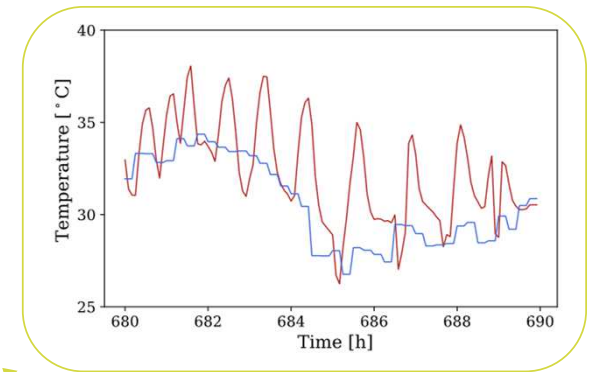
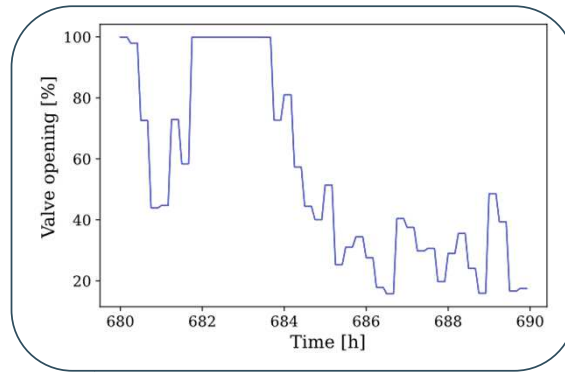
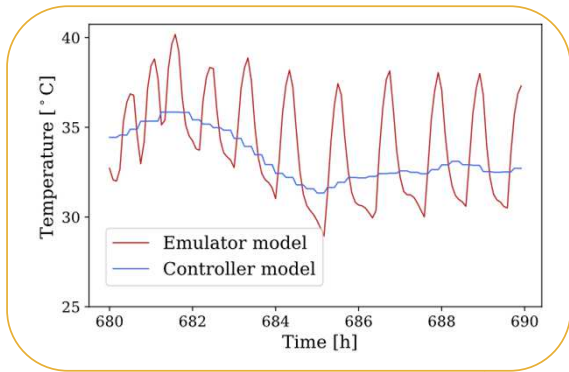
$$\left\{ \begin{array}{l} \text{HP on if } T_{WT,top} < T_{WT}^{MPC} - \Delta T_{hys,low} \\ \text{HP off if } T_{WT,bot} > T_{WT}^{MPC} + \Delta T_{hys,up} \end{array} \right.$$

2. Condenser method

$$\left\{ \begin{array}{l} \text{HP on if } T_{con,out} + \Delta T_{nom} < T_{con,out}^{MPC} - \Delta T_{hys,low} \\ \text{HP off if } T_{con,out} > T_{con,out}^{MPC} + \Delta T_{hys,up} \end{array} \right.$$

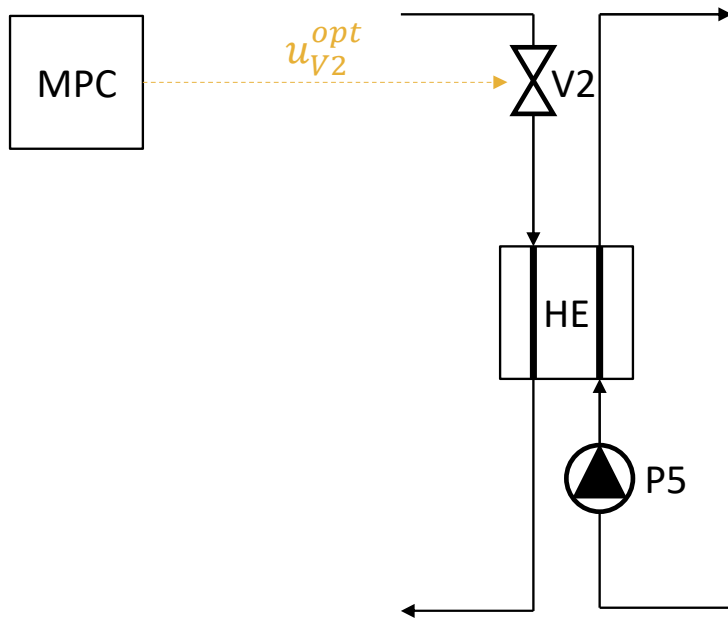


Post-processing signals – mismatch

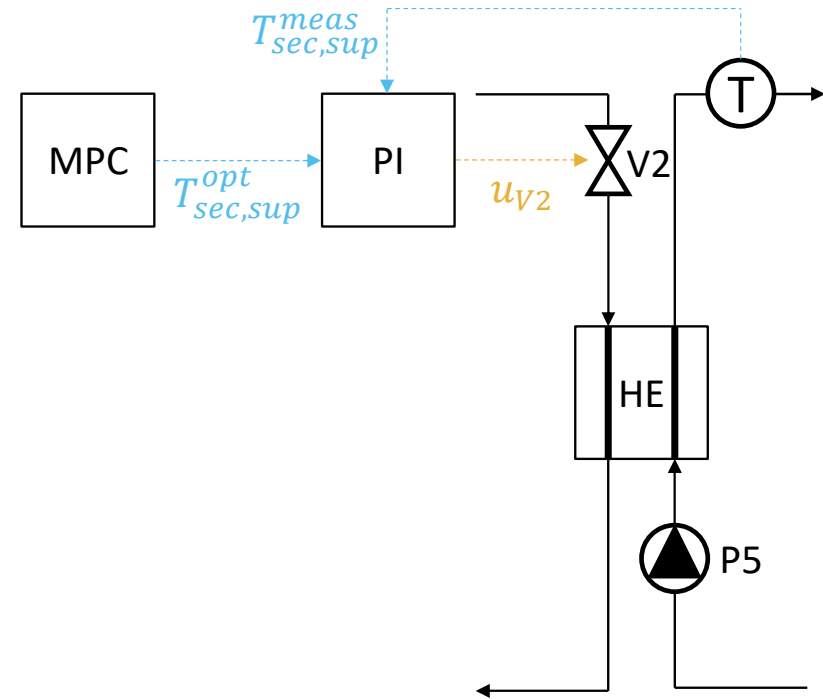


PI controller for substation valve

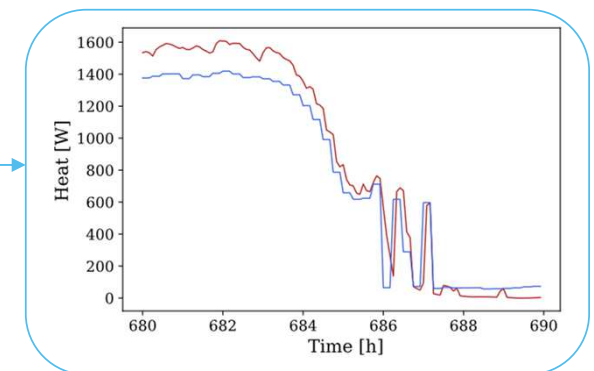
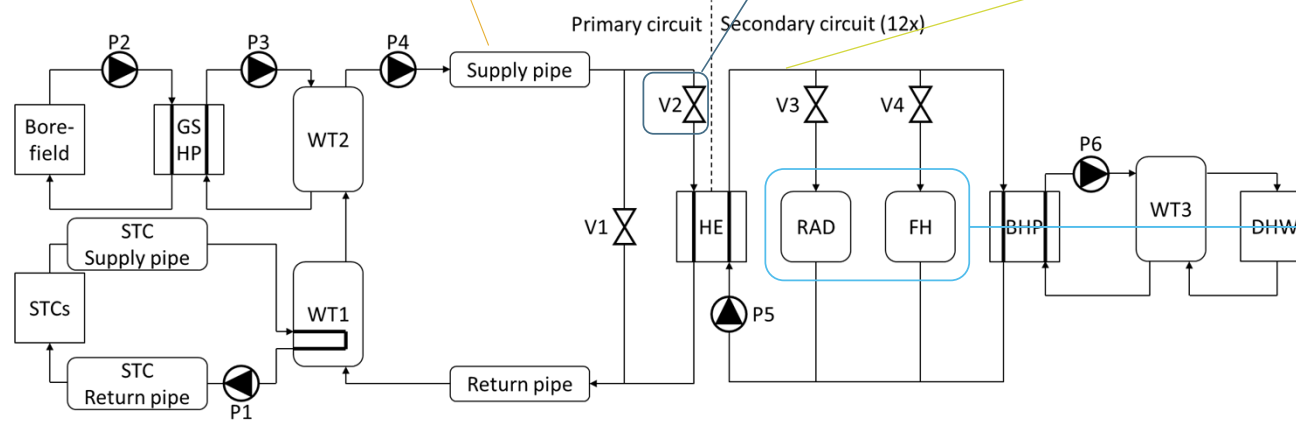
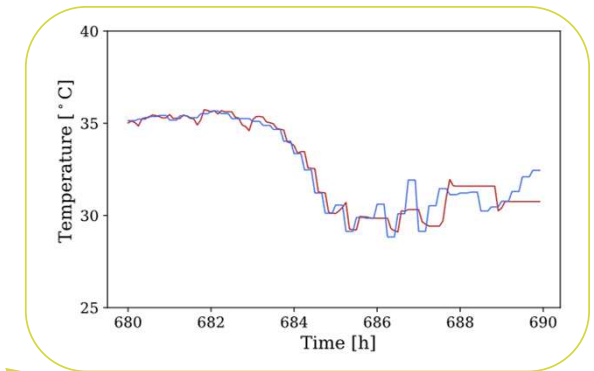
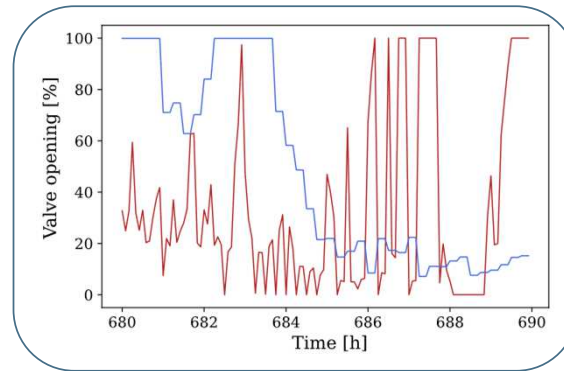
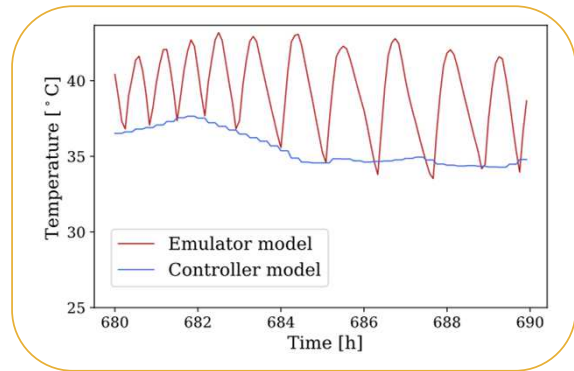
No PI controller



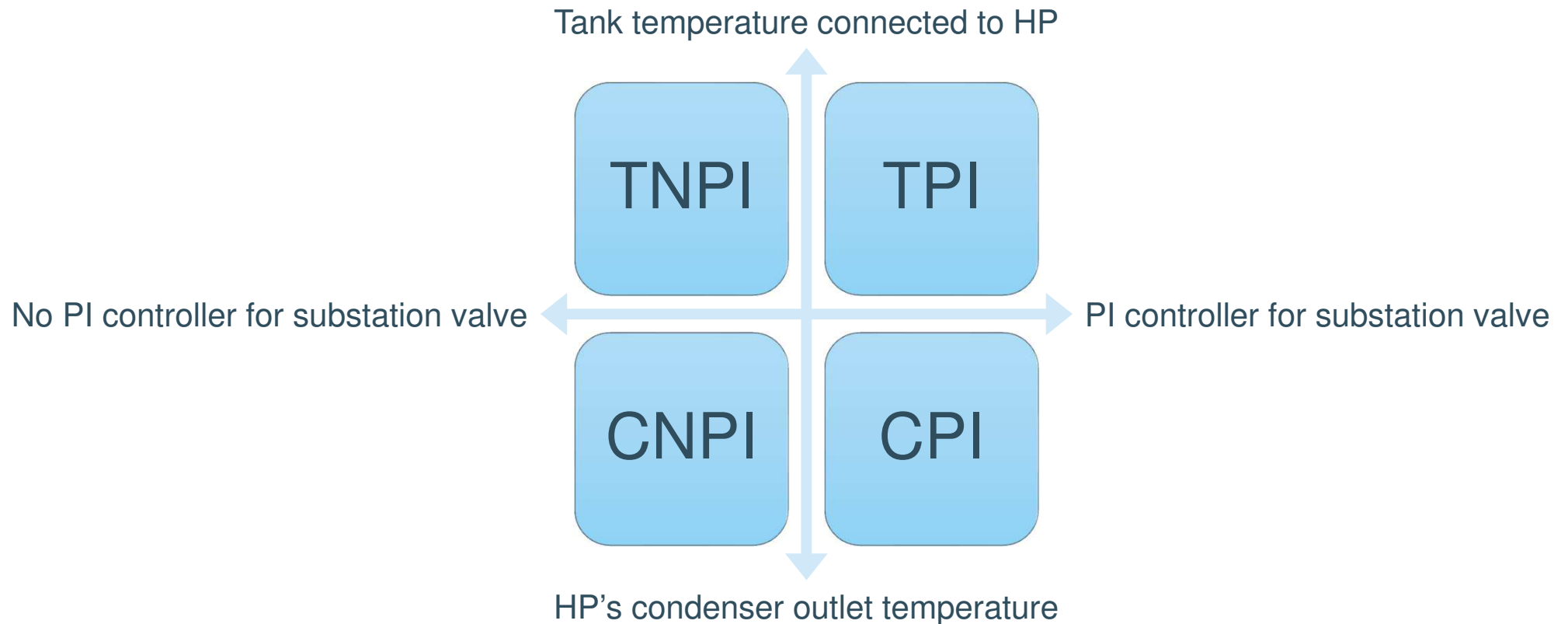
PI controller



Post-processing signals – PI controller



Post-processing methods – overview

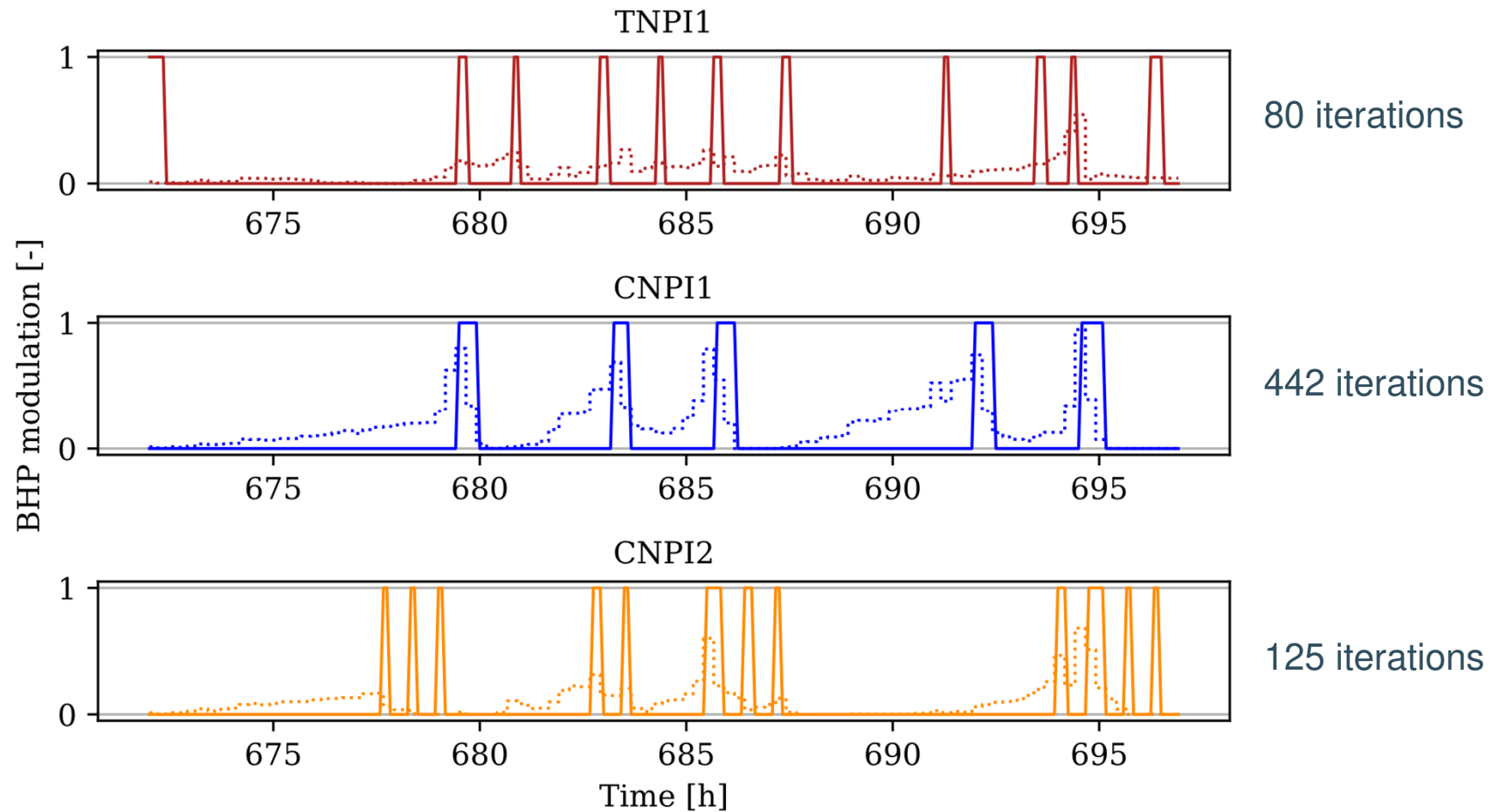


Results – tank vs. condenser approach

Simulation study of 3 days (January 28-31)

Control strategy	$\Delta T_{hys,low}$ (GSHP/BHP) [K]	$\Delta T_{hys,up}$ (GSHP/BHP) [K]	SH discomfort [Kh]	DHW discomfort [Kh]	E_{el} [kWh]	E_{HE} [kWh]	SCOP GSHP [-]	Average number of iterations
TPI1	3/0	2/3	19	0	537	1549	3.62	84
TNPI1	3/0	2/3	1	0	530	1658	3.90	80
TPI2	5/0	0/3	23	0	506	1547	3.85	82
TNPI2	5/0	0/3	34	0	503	1550	3.89	83
CPI1	0/0	8/5	17	13	526	1561	3.68	426
CNPI1	0/0	8/5	9	12	531	1630	3.78	442
CPI2	-8/-4	5/5	1	0	601	1669	3.52	125
CNPI2	-8/-4	5/5	0	0	633	1863	3.69	125
RBC	/	/	164	0	579	1501	3.31	/
Modulating	/	/	1	0	481	1651	4.71	80

Results – tank vs. condenser approach



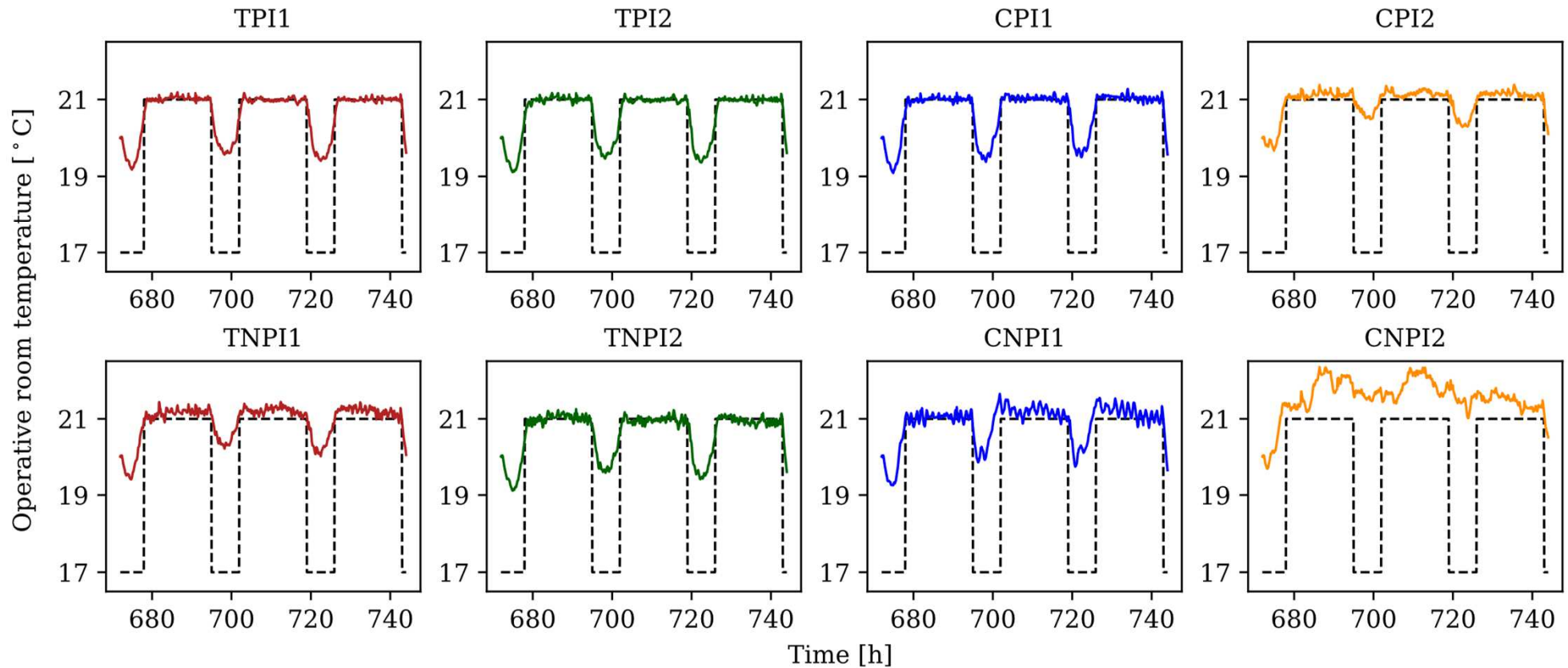
Results – tank approach

Control strategy	$\Delta T_{hys,low}$ (GSHP/BHP) [K]	$\Delta T_{hys,up}$ (GSHP/BHP) [K]	SH discomfort [Kh]	DHW discomfort [Kh]	E_{el} [kWh]	E_{HE} [kWh]	SCOP GSHP [-]	Average number of iterations
TPI1	3/0	2/3	19	0	537	1549	3.62	84
TNPI1	3/0	2/3	1	0	530	1658	3.90	80
TPI2	5/0	0/3	23	0	506	1547	3.85	82
TNPI2	5/0	0/3	34	0	503	1550	3.89	83
CP11	0/0	8/5	17	13	526	1561	3.68	426
CNPI1	0/0	8/5	9	12	531	1630	3.78	442
CP12	-8/-4	5/5	1	0	601	1669	3.52	125
CNPI2	-8/-4	5/5	0	0	633	1863	3.69	125
RBC	/	/	164	0	579	1501	3.31	/
Modulating	/	/	1	0	481	1651	4.71	80

Results – PI vs. NPI

Control strategy	$\Delta T_{hys,low}$ (GSHP/BHP) [K]	$\Delta T_{hys,up}$ (GSHP/BHP) [K]	SH discomfort [Kh]	DHW discomfort [Kh]	E_{el} [kWh]	E_{HE} [kWh]	SCOP GSHP [-]	Average number of iterations
TPI1	3/0	2/3	19	0	537	1549	3.62	84
TNPI1	3/0	2/3	1	0	530	1658	3.90	80
TPI2	5/0	0/3	23	0	506	1547	3.85	82
TNPI2	5/0	0/3	34	0	503	1550	3.89	83
CPI1	0/0	8/5	17	13	526	1561	3.68	426
CNPI1	0/0	8/5	9	12	531	1630	3.78	442
CPI2	-8/-4	5/5	1	0	601	1669	3.52	125
CNPI2	-8/-4	5/5	0	0	633	1863	3.69	125
RBC	/	/	164	0	579	1501	3.31	/
Modulating	/	/	1	0	481	1651	4.71	80

Results – operative room temperature



Results – RBC scenario

Control strategy	$\Delta T_{hys,low}$ (GSHP/BHP) [K]	$\Delta T_{hys,up}$ (GSHP/BHP) [K]	SH discomfort [Kh]	DHW discomfort [Kh]	E_{el} [kWh]	E_{HE} [kWh]	SCOP GSHP [-]	Average number of iterations
TP11	3/0	2/3	19	0	537	1549	3.62	84
TNPI1	3/0	2/3	1	0	530	1658	3.90	80
TPI2	5/0	0/3	23	0	506	1547	3.85	82
TNPI2	5/0	0/3	34	0	503	1550	3.89	83
CP11	0/0	8/5	17	13	526	1561	3.68	426
CNPI1	0/0	8/5	9	12	531	1630	3.78	442
CPI2	-8/-4	5/5	1	0	601	1669	3.52	125
CNPI2	-8/-4	5/5	0	0	633	1863	3.69	125
RBC	/	/	164	0	579	1501	3.31	/
Modulating	/	/	1	0	481	1651	4.71	80

Results – modulating HP scenario

Control strategy	$\Delta T_{hys,low}$ (GSHP/BHP) [K]	$\Delta T_{hys,up}$ (GSHP/BHP) [K]	SH discomfort [Kh]	DHW discomfort [Kh]	E_{el} [kWh]	E_{HE} [kWh]	SCOP GSHP [-]	Average number of iterations
TP11	3/0	2/3	19	0	537	1549	3.62	84
TNPI1	3/0	2/3	1	0	530	1658	3.90	80
TPI2	5/0	0/3	23	0	506	1547	3.85	82
TNPI2	5/0	0/3	34	0	503	1550	3.89	83
CPI1	0/0	8/5	17	13	526	1561	3.68	426
CNPI1	0/0	8/5	9	12	531	1630	3.78	442
CPI2	-8/-4	5/5	1	0	601	1669	3.52	125
CNPI2	-8/-4	5/5	0	0	633	1863	3.69	125
RBC	/	/	164	0	579	1501	3.31	/
Modulating	/	/	1	0	481	1651	4.71	80

Conclusion

- NLP-based MPC needs an additional post-processing step to control a DH system with integer-based input signals
 - Post-processing step
 - Suboptimality
 - Ad hoc approach
- ➔ MINLP-based MPC
- No loss of optimality due to post-processing
 - Reduce model mismatch

Questions?

Additional slides

Simulation study

- 3 days (January 28-31)

- MPC

- $\Delta t_{prediction} = 2$ days
- $\Delta t_{control} = 15$ minutes
- Perfect predictions

- Metrics

- SH discomfort = $\int_{t_{start}}^{t_{end}} \max(0, (T_{in}^{set} - 1) - T_{in}) dt$
- DHW discomfort = $\int_{t_{start}}^{t_{end}} [\text{if } \dot{m}_{DHW} > 0 \text{ then } \max(0, (T_{DHW}^{set} - 1) - T_{DHW}) \text{ else } 0] dt$
- Electricity use E_{el}
- SCOP GSHP
- Substation heat E_{HE}
- Average # iterations optimiser

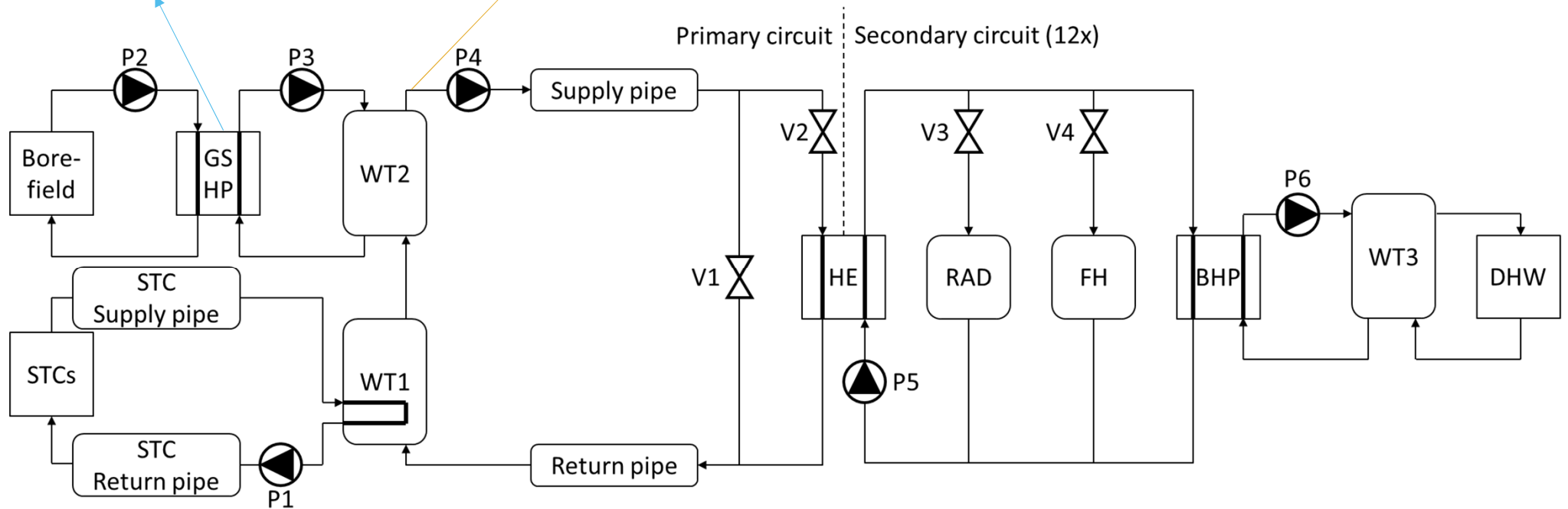
Results – PI vs. NPI

Control strategy	$\Delta T_{hys,low}$ (GSHP/BHP) [K]	$\Delta T_{hys,up}$ (GSHP/BHP) [K]	SH discomfort [Kh]	DHW discomfort [Kh]	E_{el} [kWh]	E_{HE} [kWh]	SCOP GSHP [-]	Average number of iterations
TPI1	3/0	2/3	19	0	537	1549	3.62	84
TNPI1	3/0	2/3	1	0	530	1658	3.90	80
TPI2	5/0	0/3	23	0	506	1547	3.85	82
TNPI2	5/0	0/3	34	0	503	1550	3.89	83
CPI1	0/0	8/5	17	13	526	1561	3.68	426
CNPI1	0/0	8/5	9	12	531	1630	3.78	442
CPI2	-8/-4	5/5	1	0	601	1669	3.52	125
CNPI2	-8/-4	5/5	0	0	633	1863	3.69	125
RBC	/	/	164	0	579	1501	3.31	/
Modulating	/	/	1	0	481	1651	4.71	80

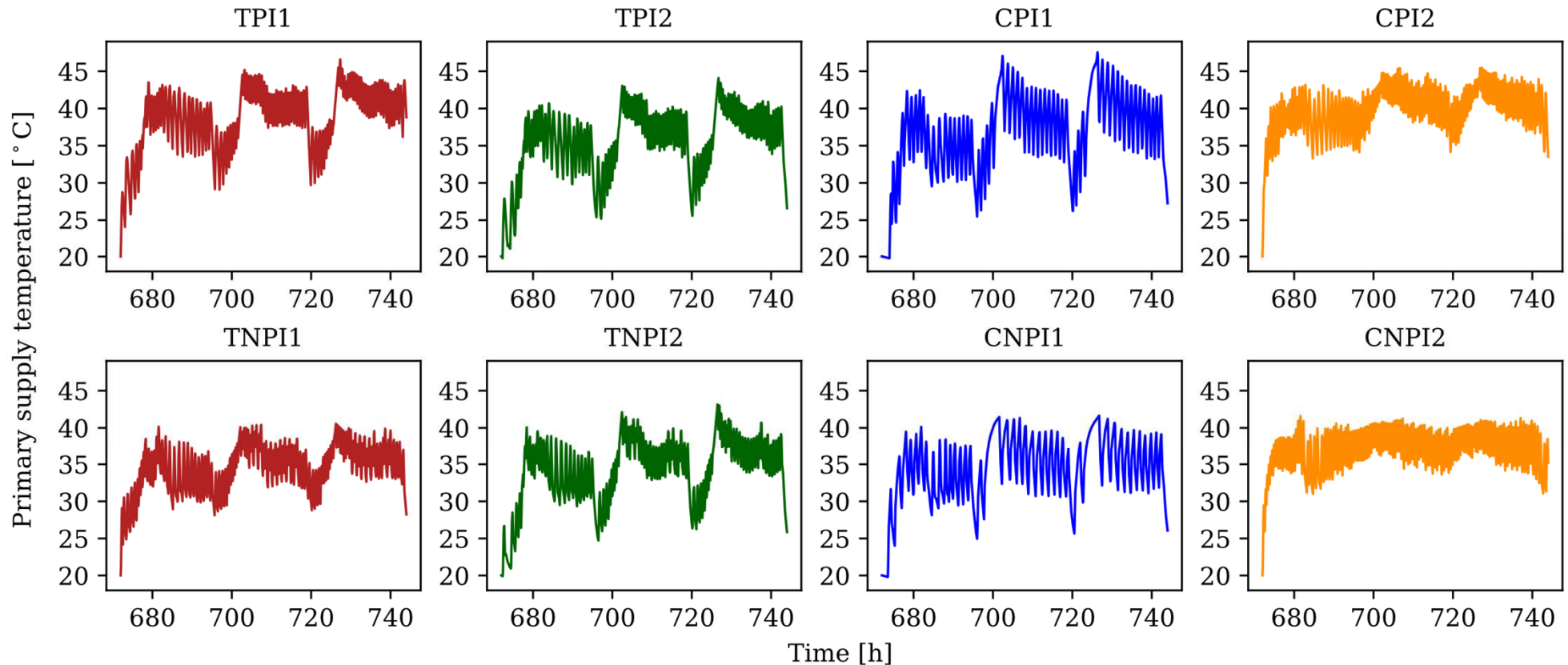
Results – PI vs. NPI – SCOP

$$COP_{GSHP} \sim 1/T_{con}$$

$$T_{con} \sim T_{WT2} \sim T_{prim,sup}$$



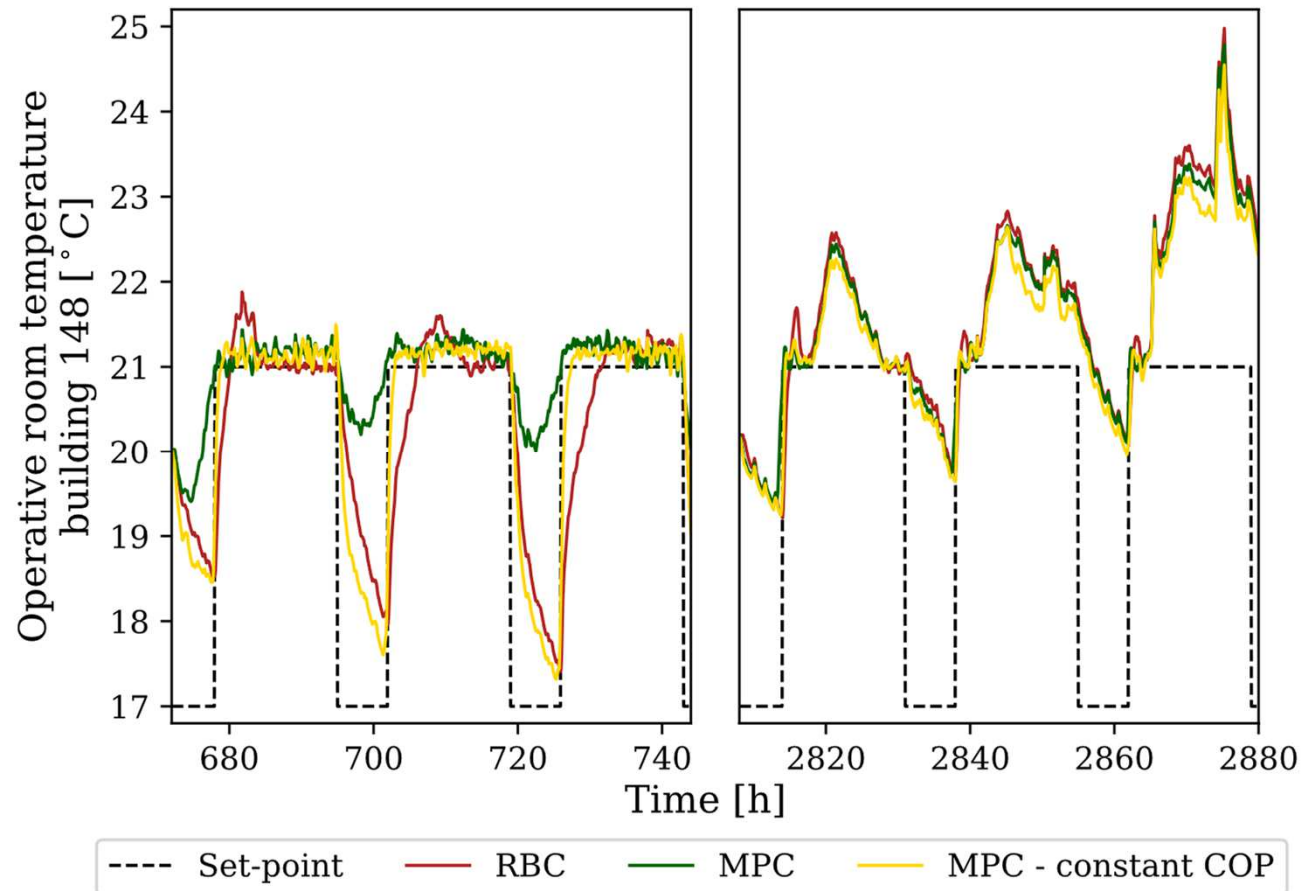
Results – primary supply temperature



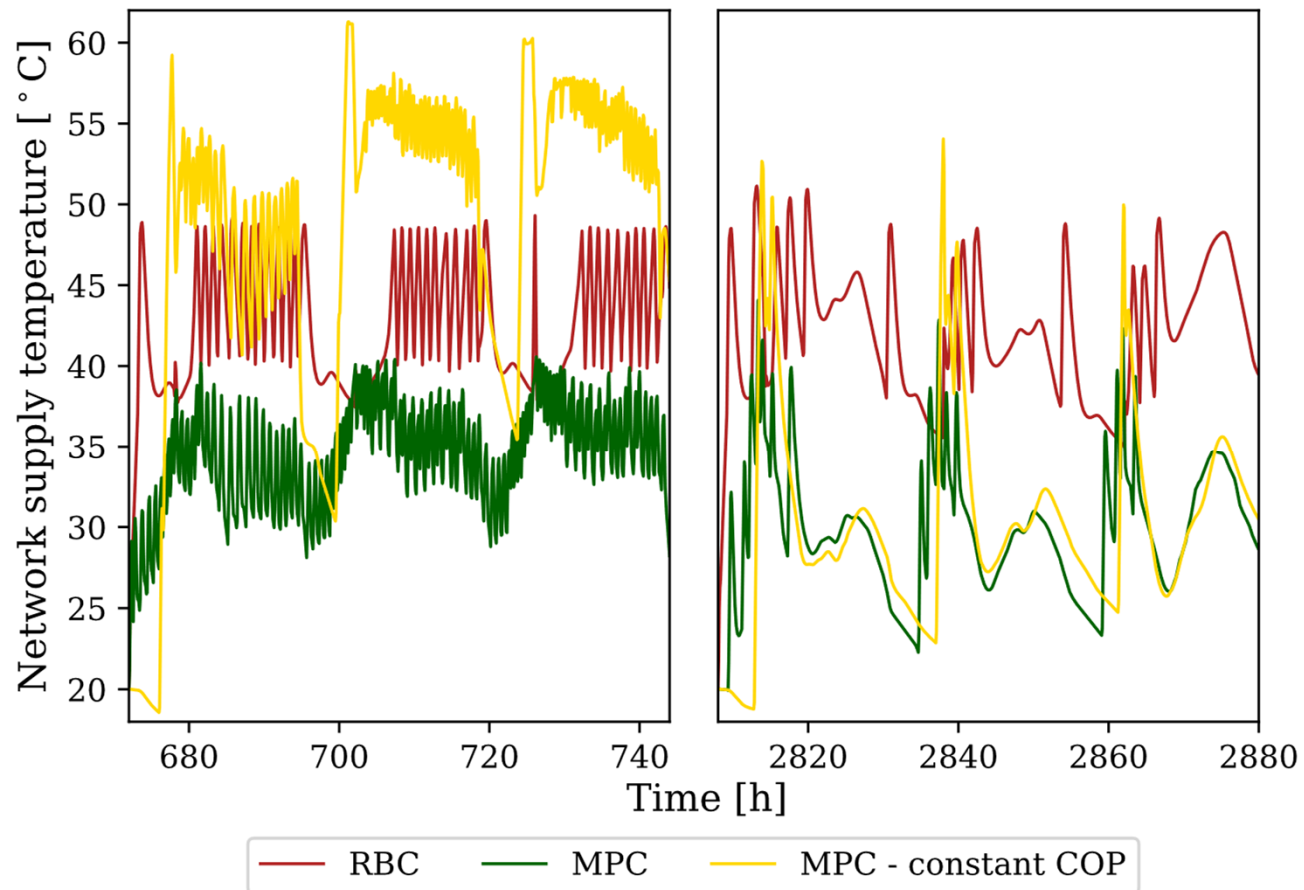
MPC vs. RBC

Control strategy	SH discomfort [Kh]	DHW discomfort [Kh]	Electricity use [kWh]			Heat demand [kWh]		SCOP [-]	
			$E_{el,tot}$	$E_{GSHP,el}$	$E_{BHP,el}$	E_{HE}	$E_{distr,loss}$	GSHP	BHP
Winter									
RBC	164	0	579	509 (88%)	36 (6%)	1500	126	3.31	3.63
MPC	1	0	530	456 (86%)	29 (5%)	1657	107	3.90	3.87
MPC – constant COP	25	0	720	636 (88%)	49 (7%)	1431	144	2.52	2.65
Spring									
RBC	21	0	165	115 (69%)	40 (24%)	343	117	3.62	3.62
MPC	2	0	119	65 (54%)	41 (34%)	319	83	4.29	3.14
MPC – constant COP	8	0	141	71 (51%)	56 (40%)	279	84	3.51	2.49

Operative room temperature



Network supply temperature



DHW supply temperature

