



Valorisation of biogas digestate through nutrient recovery by means of membrane distillation - The “BioProfit” project



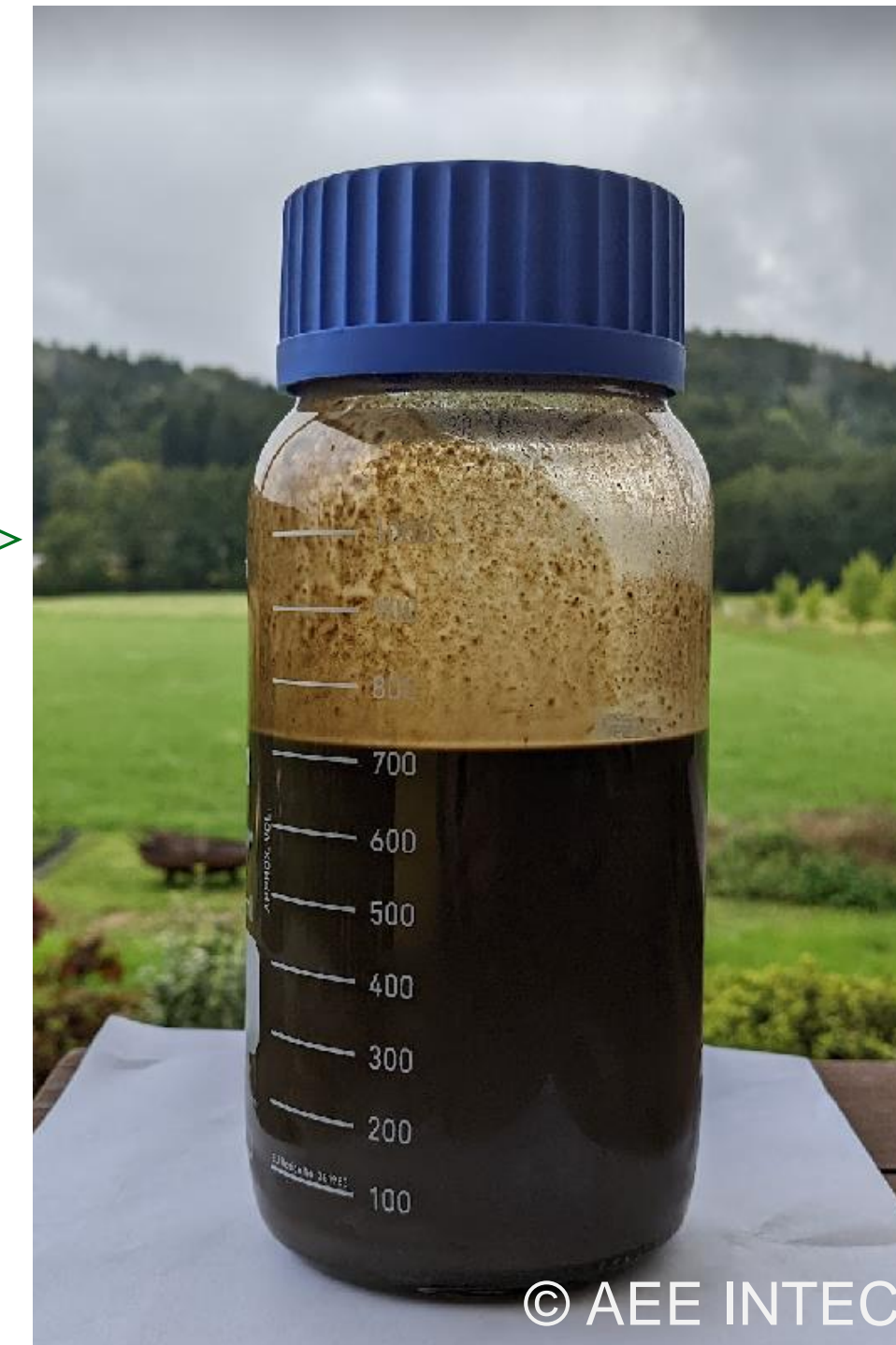
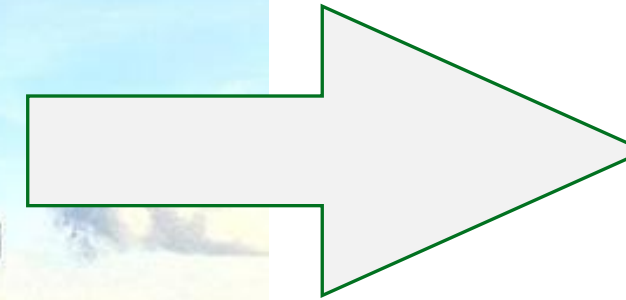
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DI (FH) Christian Platzer MSc.
DI Dr. Bettina Muster-Slawitsch

BioProfit
Profitable Valorisation von
Biogasgärresten durch CO₂-Speicherung
und Nährstoffrückgewinnung



Initial Situation ACR - BioProfit Project

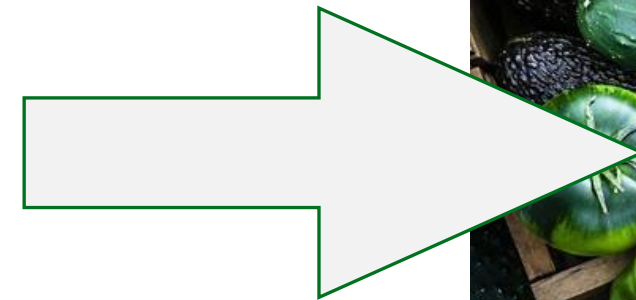


- Around 20,000 biogas plants are in operation in Europe

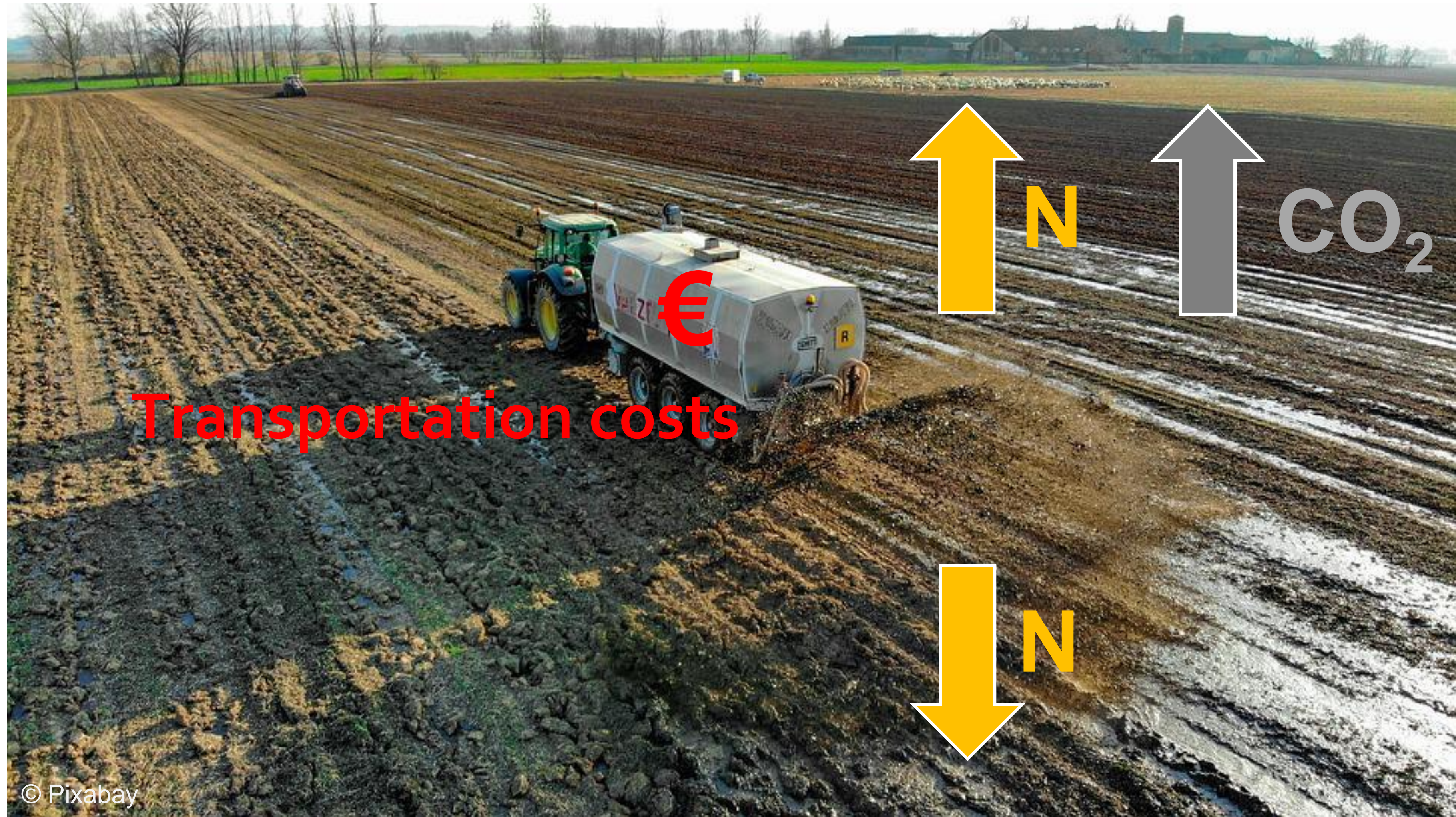


Without macronutrients (NPK) - no plant growth

Carbon
Nitrogen – N
Phosphorus – P
Potassium - K

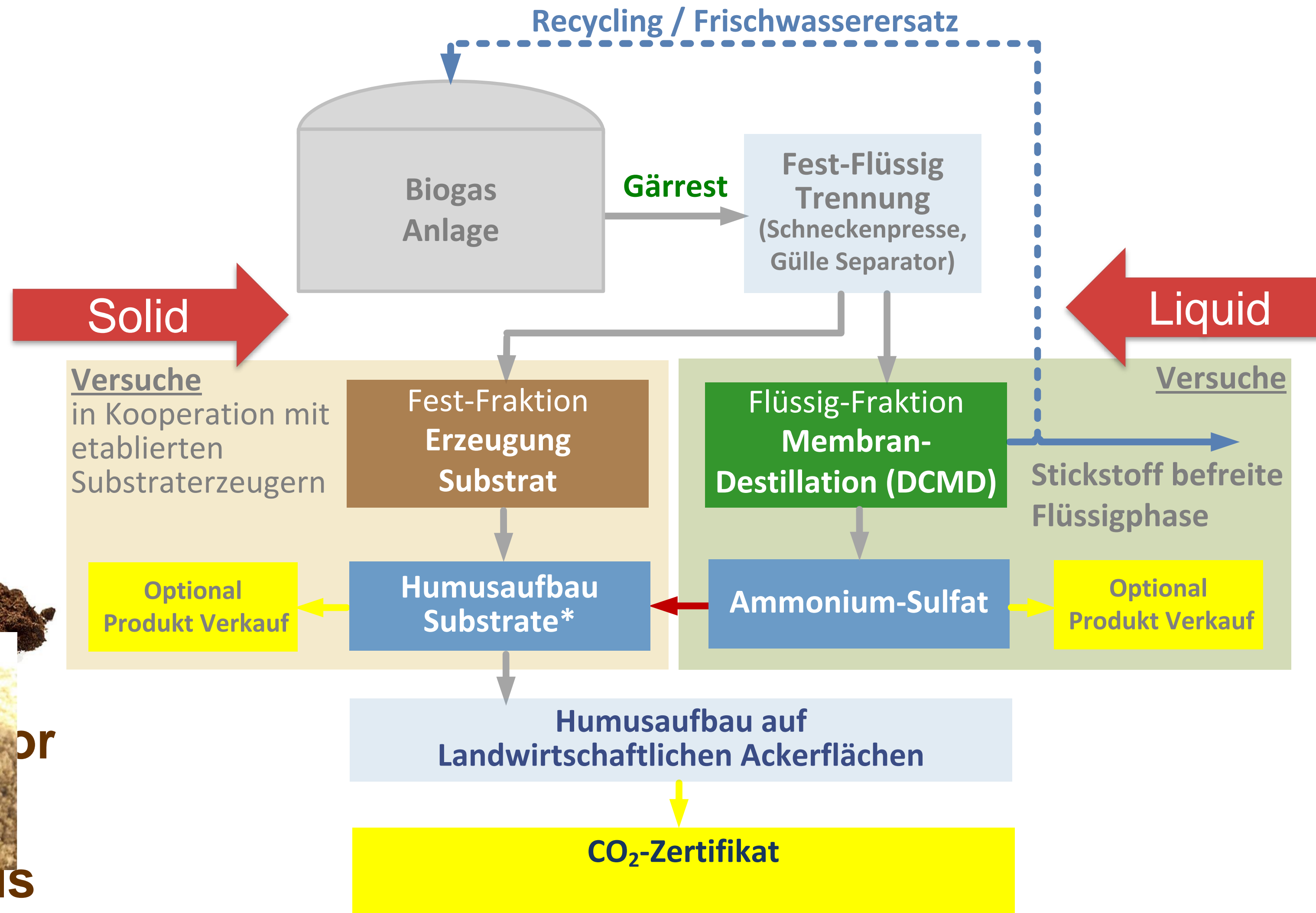


Status Quo! - Disposal of biogas fermentation residues



Visualization of the "BioProfit" solution concept

C + NPK



Revenues (€)



N-Recycling

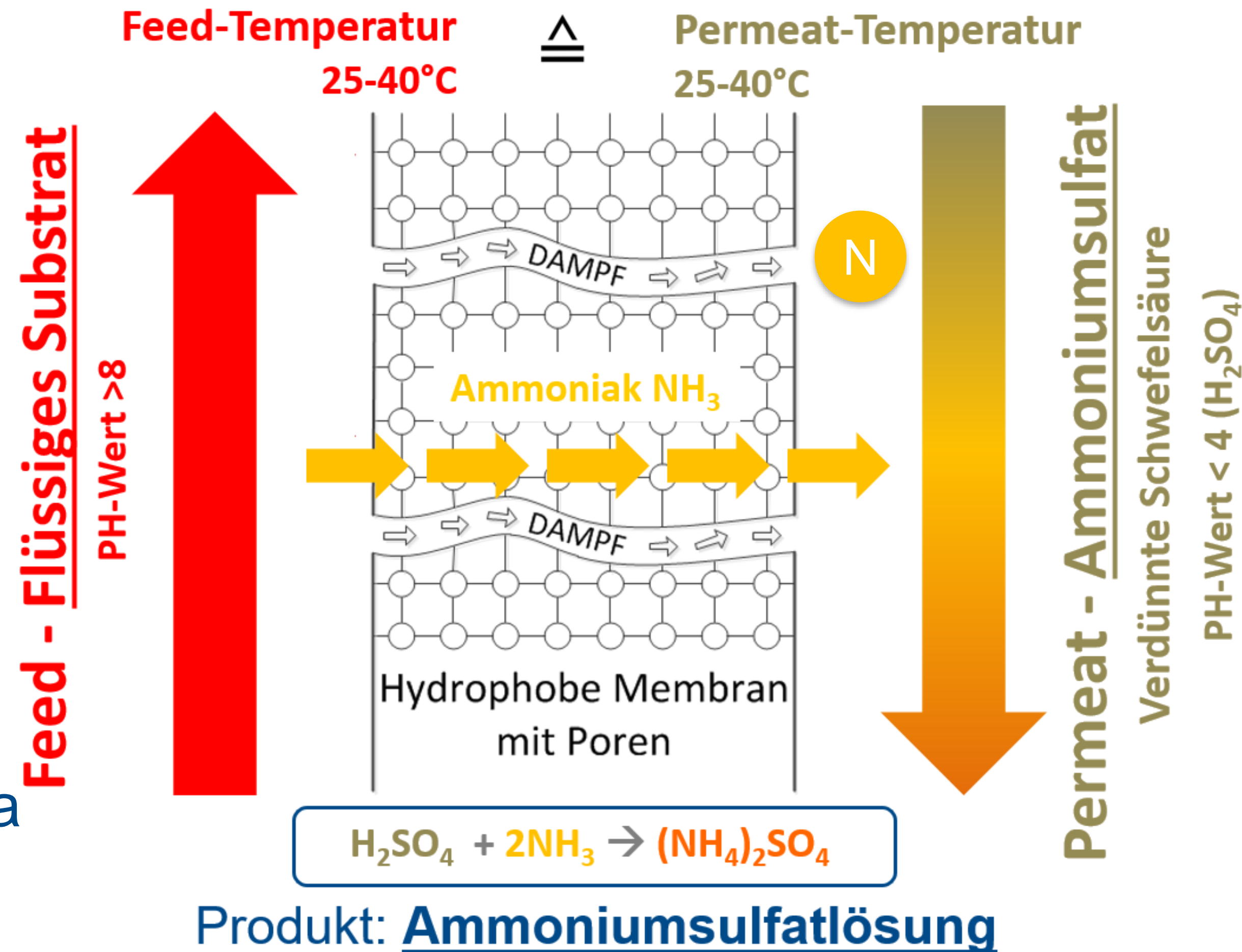
Liquid fertilizer



Membrane distillation process Product generation of ammonium sulphate using **isothermal DCMD**



Membrane distillation (MD) is a thermally driven separation / concentration process



Revenue Product (€)





Solid fraction



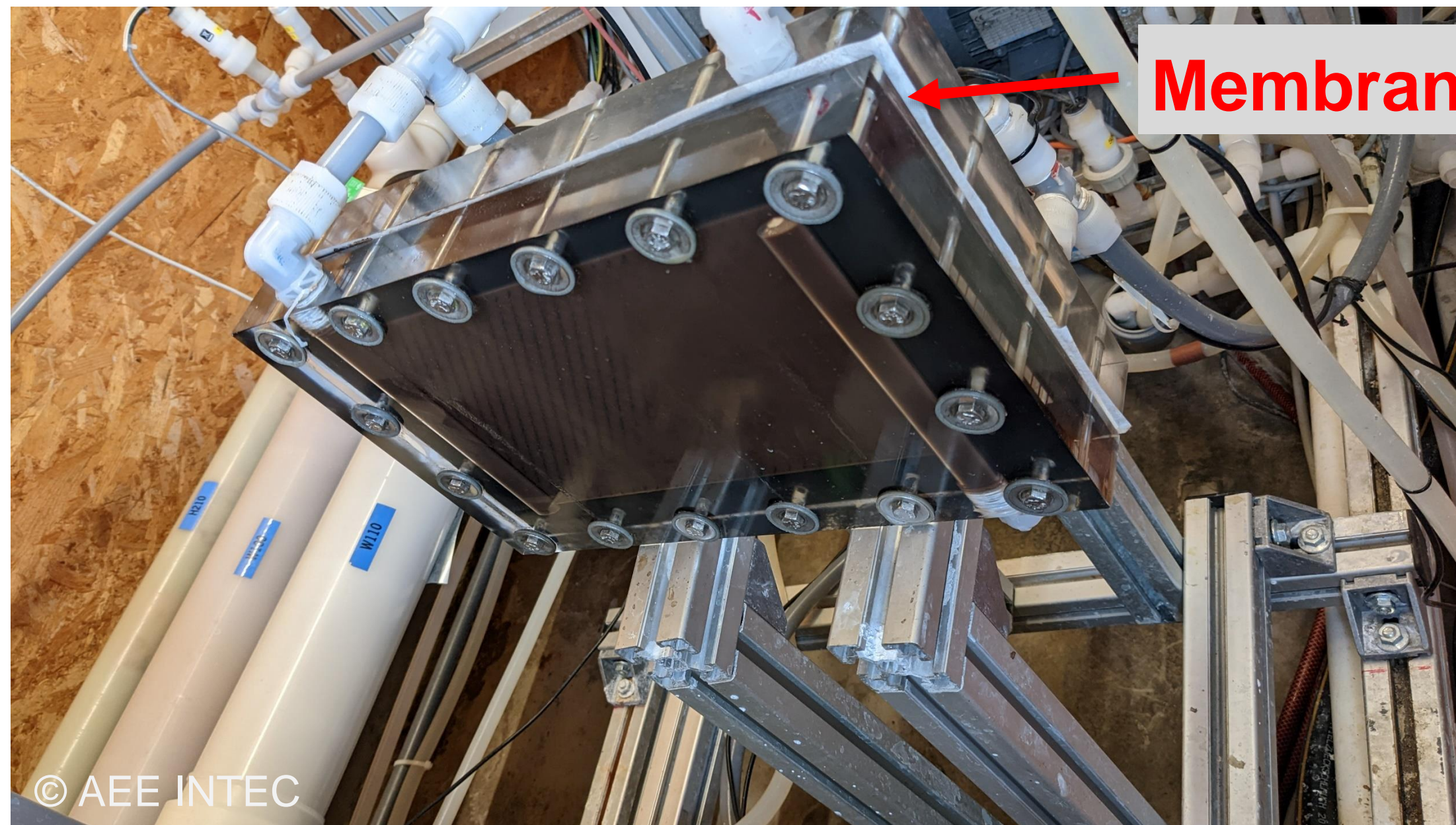
Liquid fraction

Phase I

Preliminary tests with an MD membrane test cell

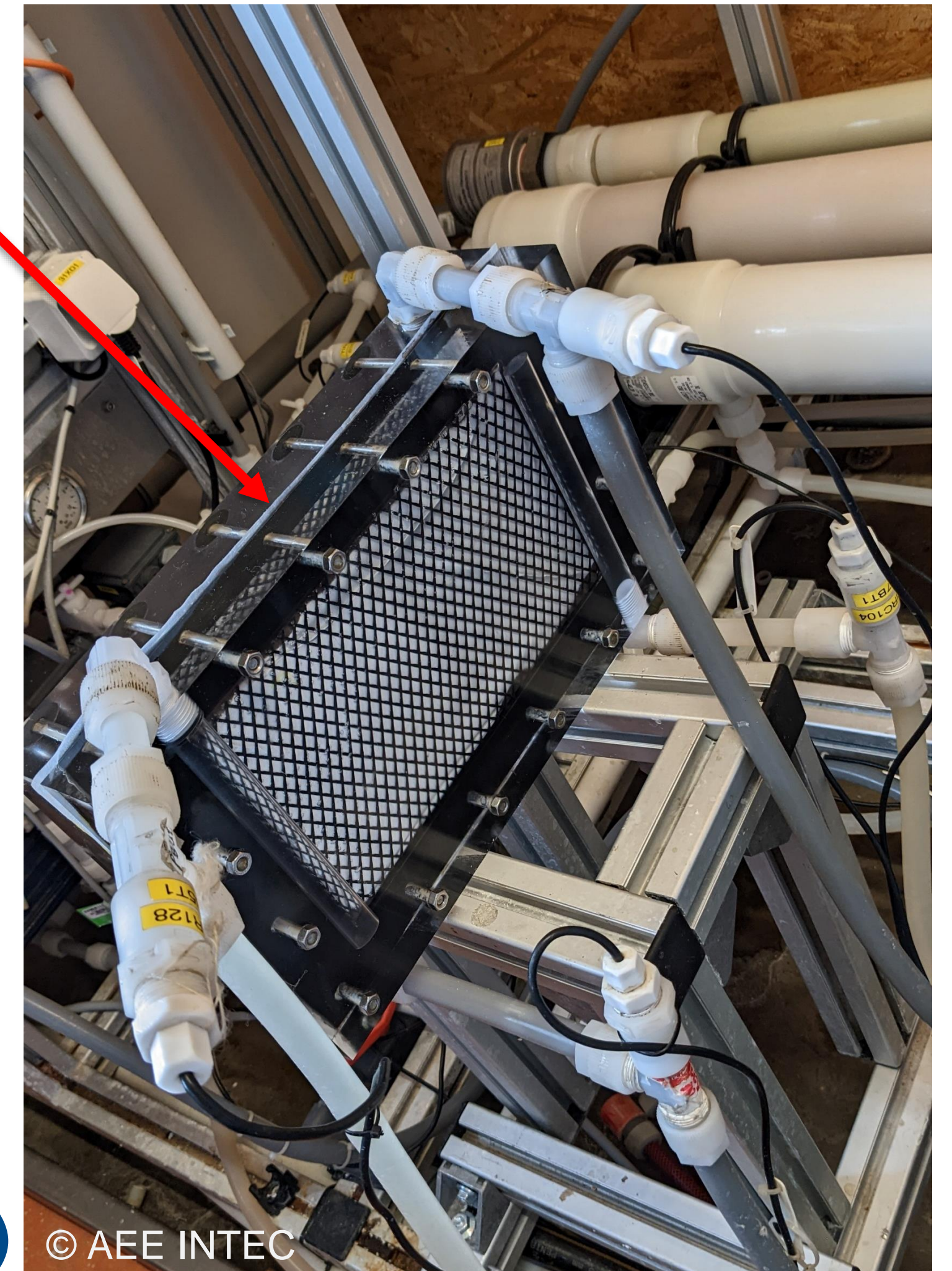


Preliminary tests with an MD membrane test cell in the laboratory

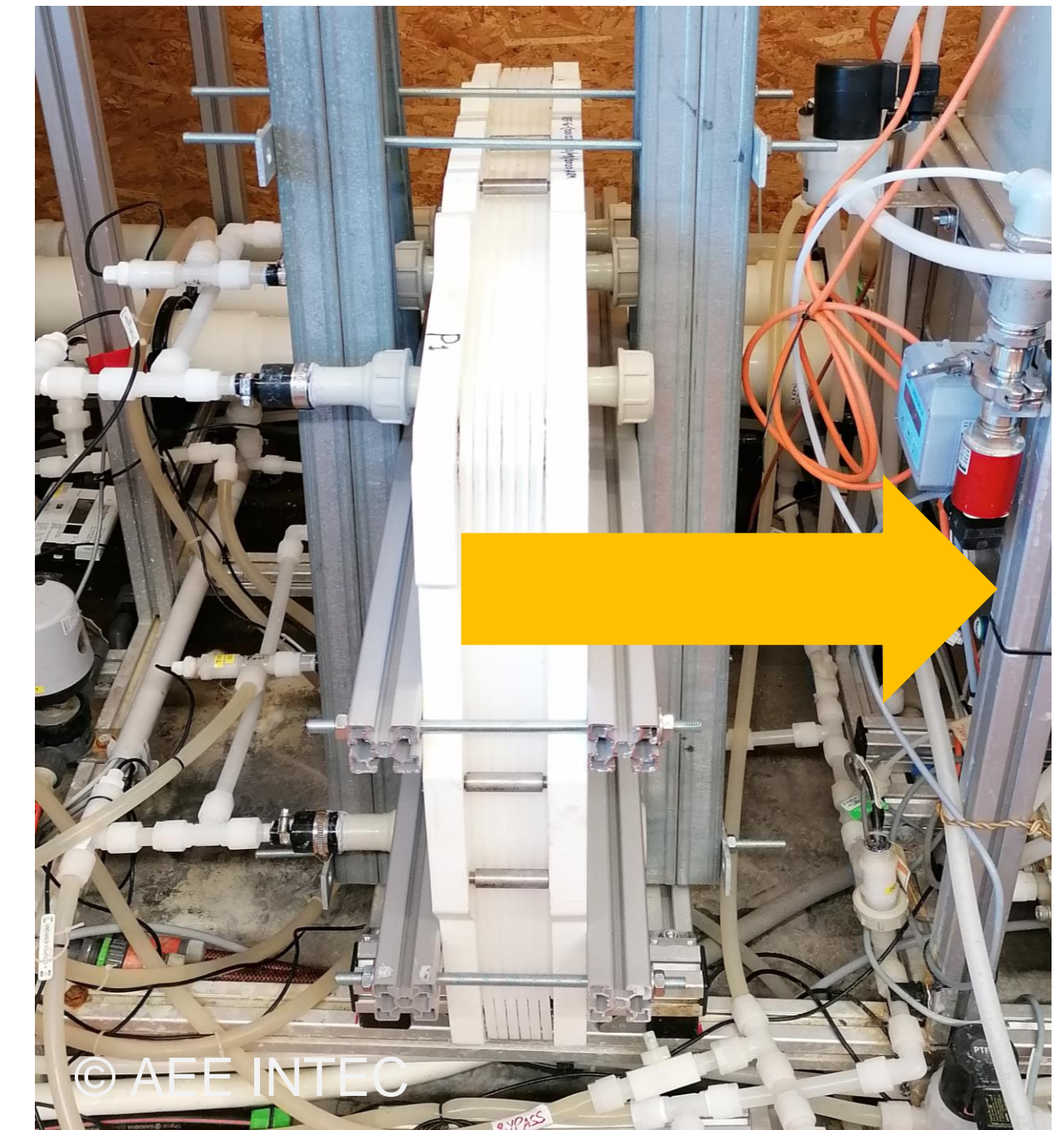


Feed side (digestate)

**Permeate side
(high-purity ammonium sulphate solution)**



Phase II - Endurance test 24/7 with the MD container system and large-scale membrane modules



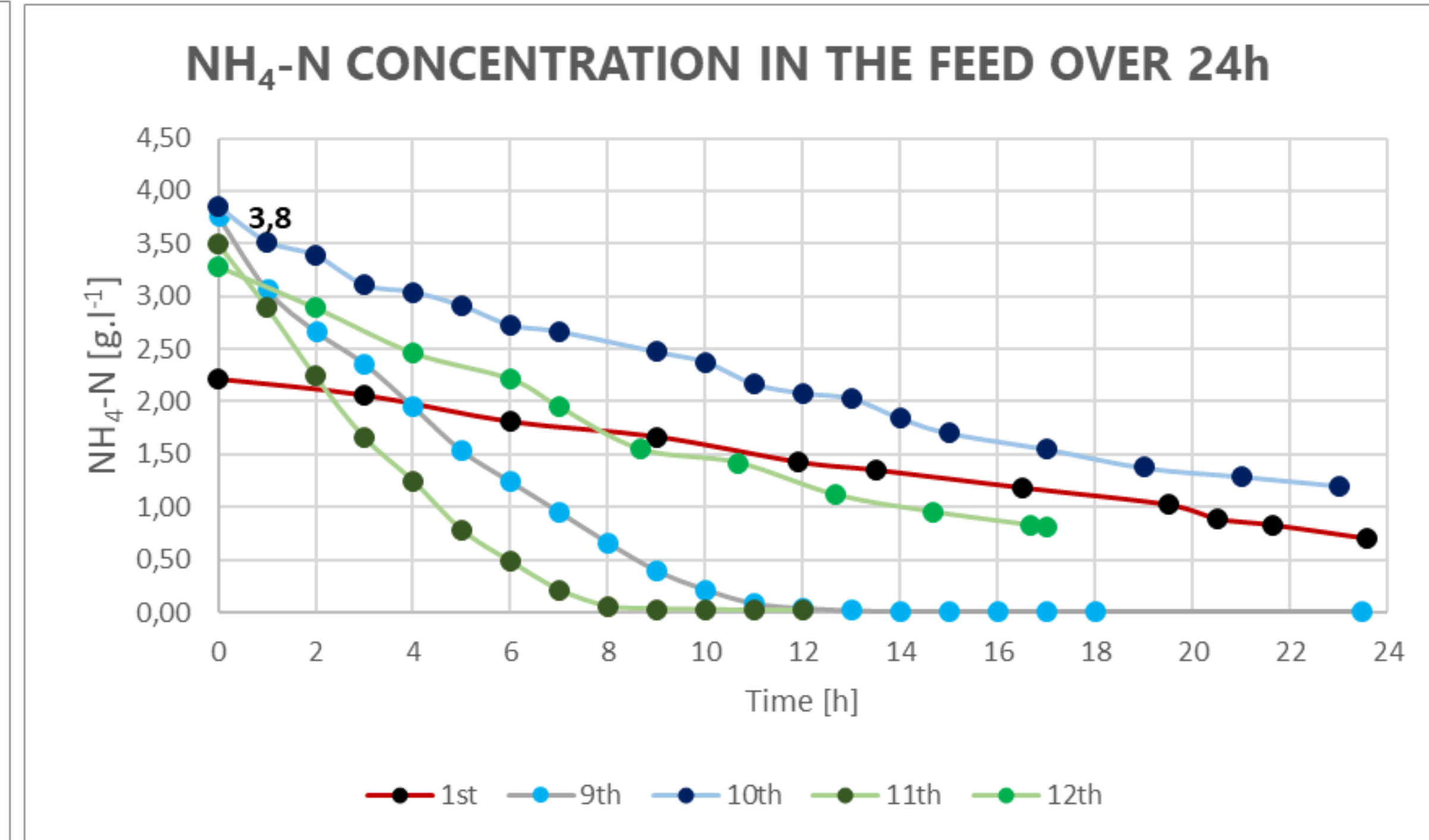
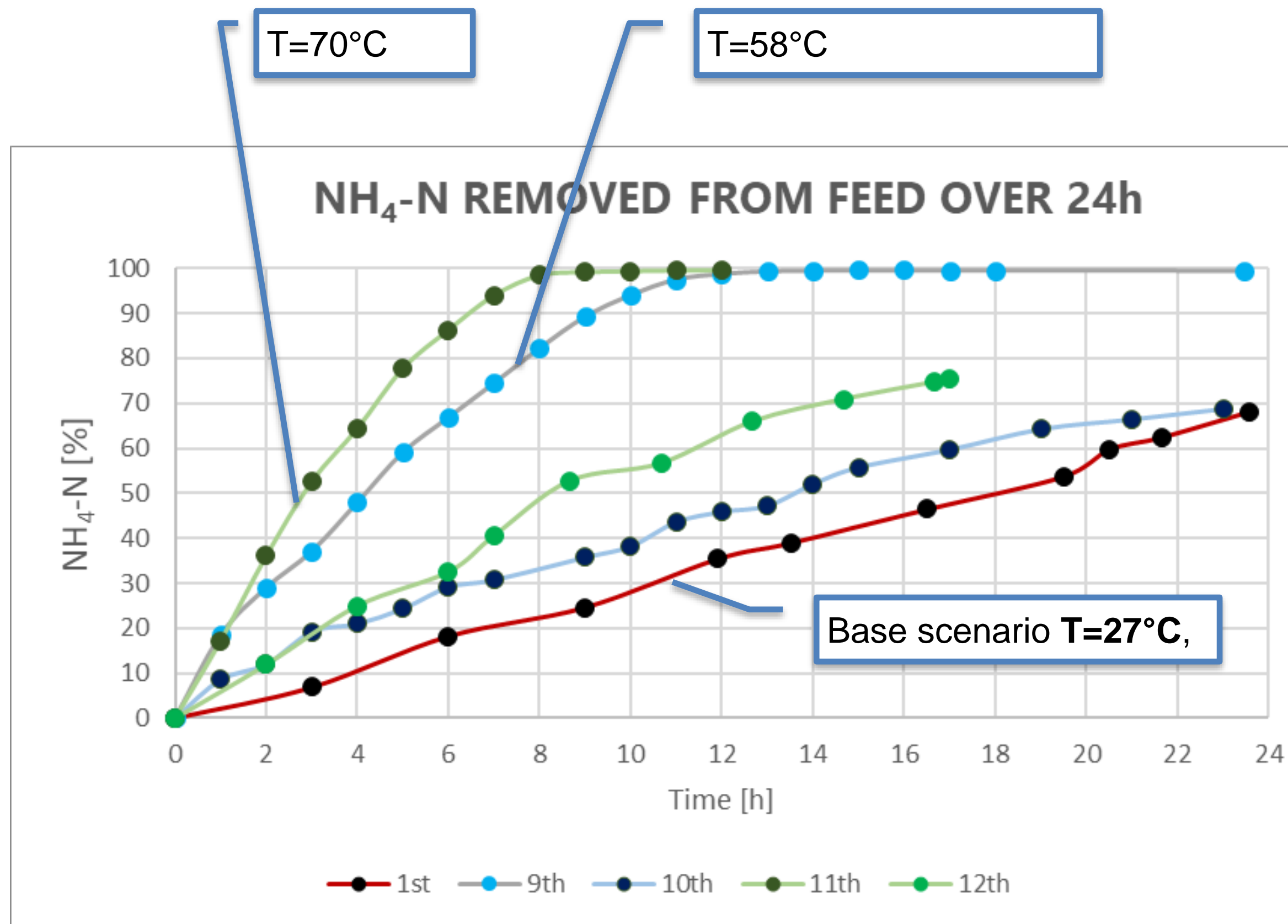
Endurance test TARGET: NH₄-N reduction in fermentation residue

- Extensive NH₄-N reduction possible even at a low temperature level of 27°C

[Text]	[h]	[%]	[%]
Samples	Abs time	NH ₄ -N retained	NH ₄ -N removed
F0	0	100,00	0,00
F1	3,00	93,13	6,87
F2	6,00	81,79	18,21
F3	9,00	75,39	24,61
F4	11,90	64,64	35,36
F5	13,52	61,06	38,94
F6	16,52	53,57	46,43
F7	19,52	46,24	53,76
F8	20,52	40,22	59,78
F9	21,65	37,61	62,39
F10	23,58	31,91	68,09
F11	26,58	27,14	72,86
F12	29,58	21,35	78,65
F13	32,58	16,07	83,93
F14	35,58	10,25	89,75
F15	47,58	1,34	98,66
F16	50,58	1,10	98,90
F17	53,58	0,91	99,09
F18	56,58	0,86	99,14
F19	59,58	0,85	99,15

Acceleration of the process by raising the temperature

1st average $J_{\text{flux}} \text{ NH}_4\text{-N} \sim 2 \text{ [g.m}^{-2}\text{.h}^{-1}]$
 11th average $J_{\text{flux}} \text{ NH}_4\text{-N} \sim 18,8 \text{ [g.m}^{-2}\text{.h}^{-1}]$

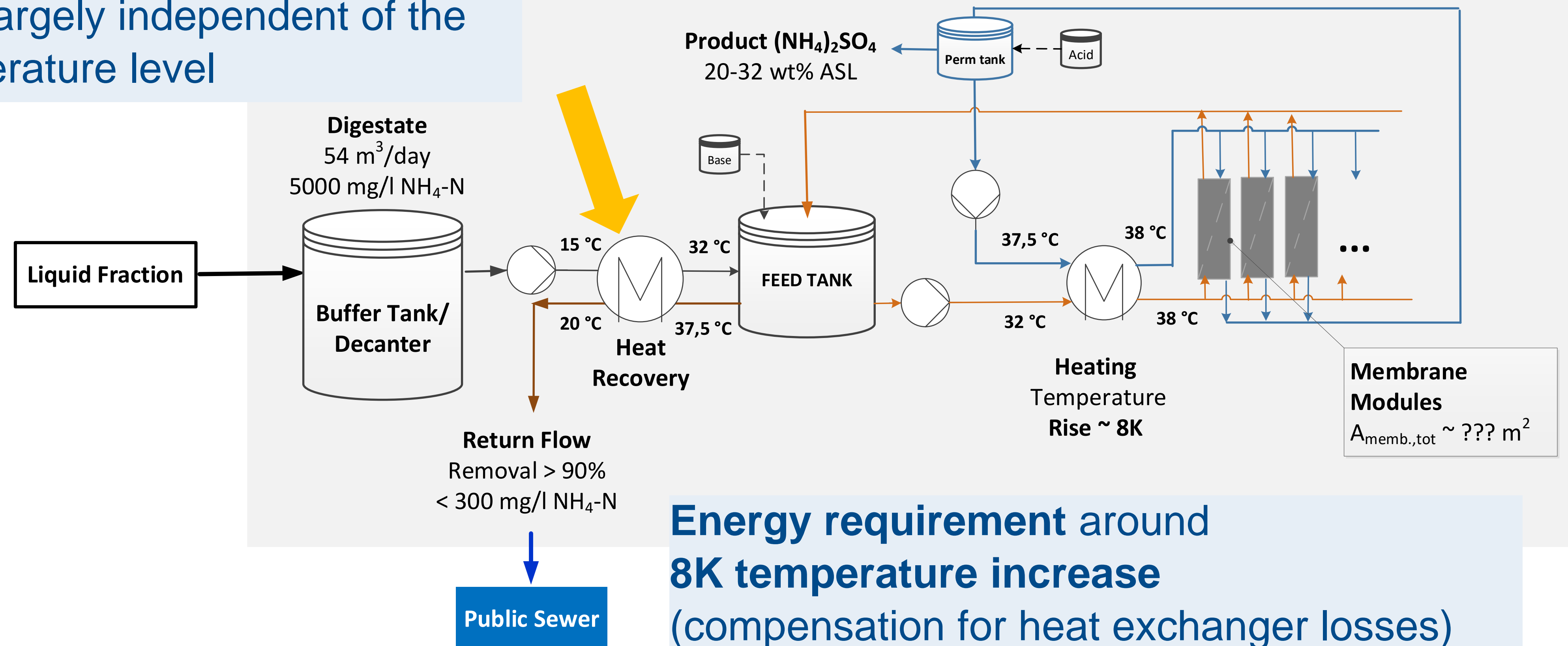


Saving thermal energy requirements through heat recovery

Heat recovery means that the energy requirement is largely independent of the operating temperature level

Göss – MD Plant Concept

- Draft Concept -



Energy requirement around 8K temperature increase
(compensation for heat exchanger losses)

Sum –Up Development Phase I and Phase II

- The **quality targets** were achieved without any problems
- The MD process has proven to be very robust for liquids containing large amounts of particles. The process is operated at atmospheric pressure, the membrane is flooded with virtually **no pressure** and the ammonia evaporates true the membrane.
 - No particles are pressed into the membrane pores
- **Uncomplicated pre-treatment**; Mechanical solid/liquid separation of the fermentation residue and settling tank are sufficient for pre-treatment
- Use of **flocculants** (high chemical cost!) **are not required**
- The **optimum operating conditions** depend on the implementation situation and the concept of the respective biogas plant (waste heat availability). Trade-off between N-flow, operating temperature and operating costs (i.e. chemical costs)

➤ Next Steps:

- Start of **Phase III** - the pilot phase together with a biogas plant manufacturer (BIOGEST - Vienna)
- Further research: Development of an organic-certifiable liquid fertilizer by using biogenic acidifiers

Thank you !

BioProfit

Profitable Valorisation von
Biogasgärresten durch CO₂-Speicherung
und Nährstoffrückgewinnung

a_{cr} austrian
cooperative
research





AEE INTEC

IDEA TO ACTION

AEE – Institute for Sustainable Technologies (AEE INTEC)
8200 Gleisdorf, Feldgasse 19, Austria

Website: www.aee-intec.at
Twitter: @AEE_INTEC

Christian Platzer
c.platzer@aee.at
+43 3112 / 58 86 - 522